

# The Impossible Triangle:

Balancing Quality, Efficiency, and Cost  
Can You Really Have It All?

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# OUTLINE

## **1. Fargo Water Utility Overview**

- Water Treatment Plant Overview
- Raw Water
- Plant Performance

## **2. Impossible Triangle**

- Quality
- Efficiency
- Cost

## **3. Strategies and Innovations to Get the Job Done**

# Fargo Water Utility Overview





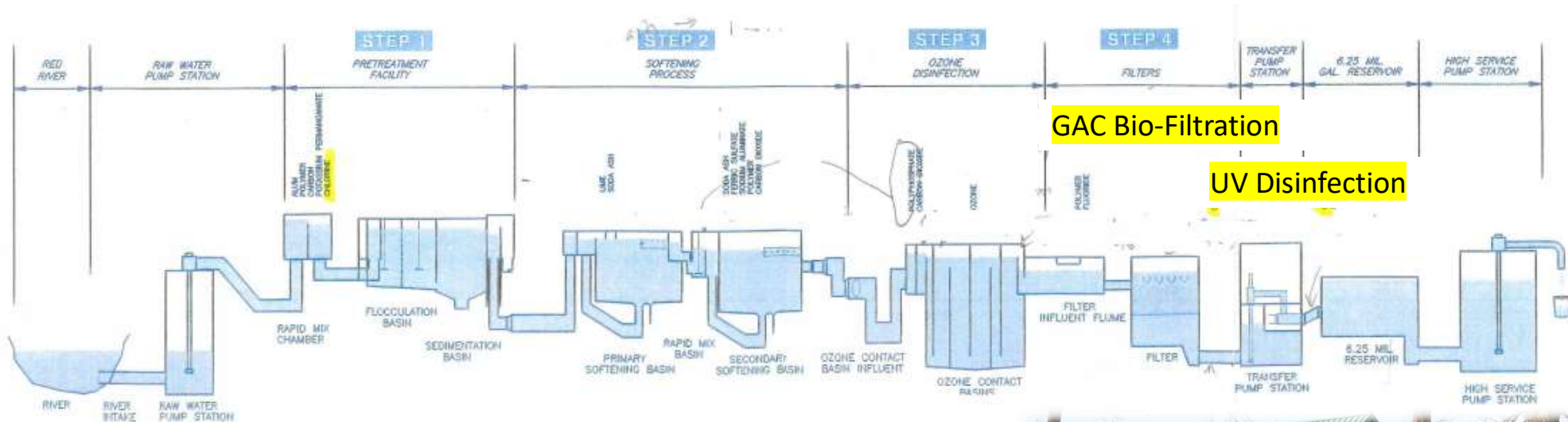
- **30 MGD Lime Softening WTP (1997)**

- **15 MGD Integrated Duo Membrane WTP (2018)**



# Fargo Lime Softening WTP

- Fargo Water Treatment Plant (WTP) in operation since 1912
- Current WTP completed in 1997 with a capacity of 30 million gallons per day (mgd)

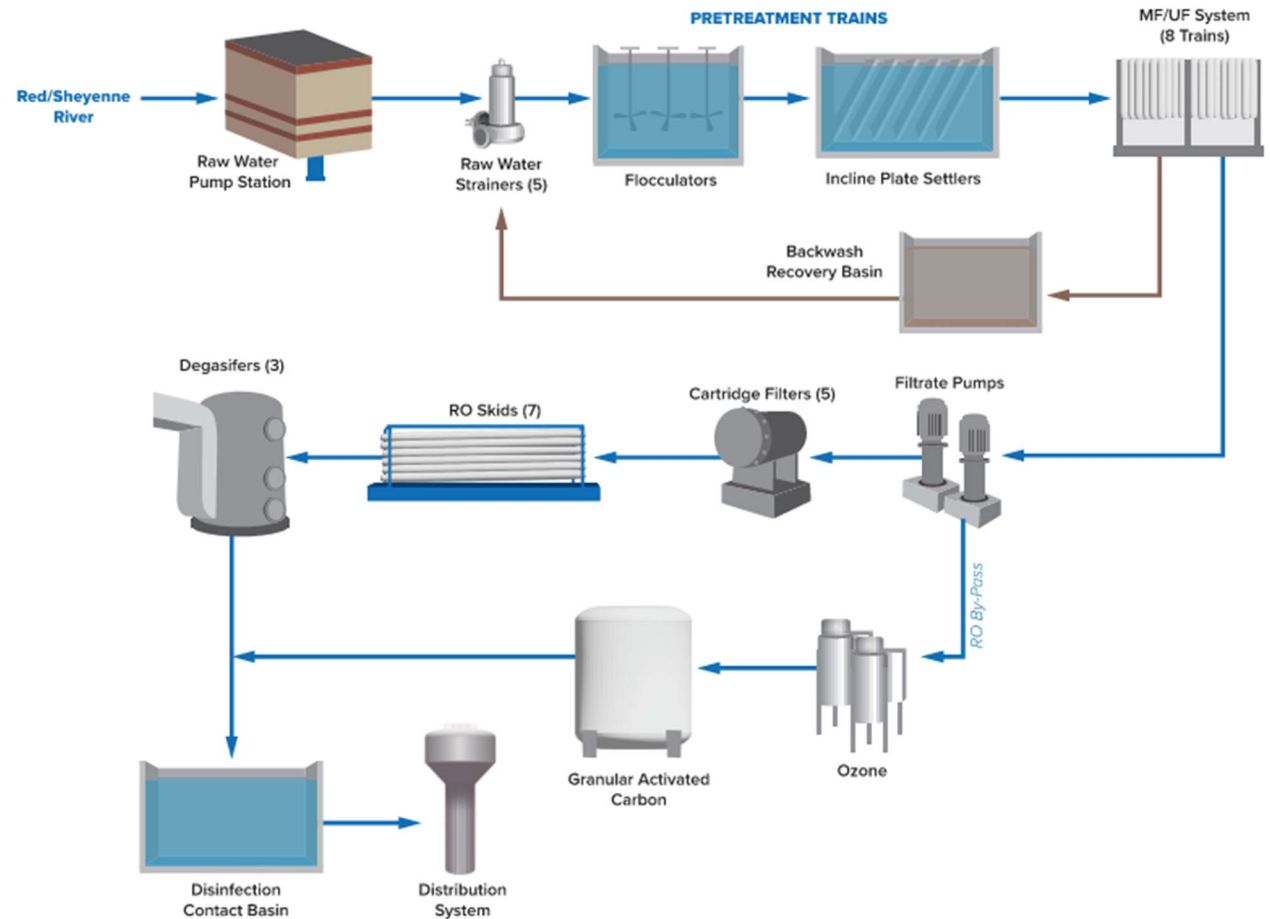


GAC Bio-Filtration

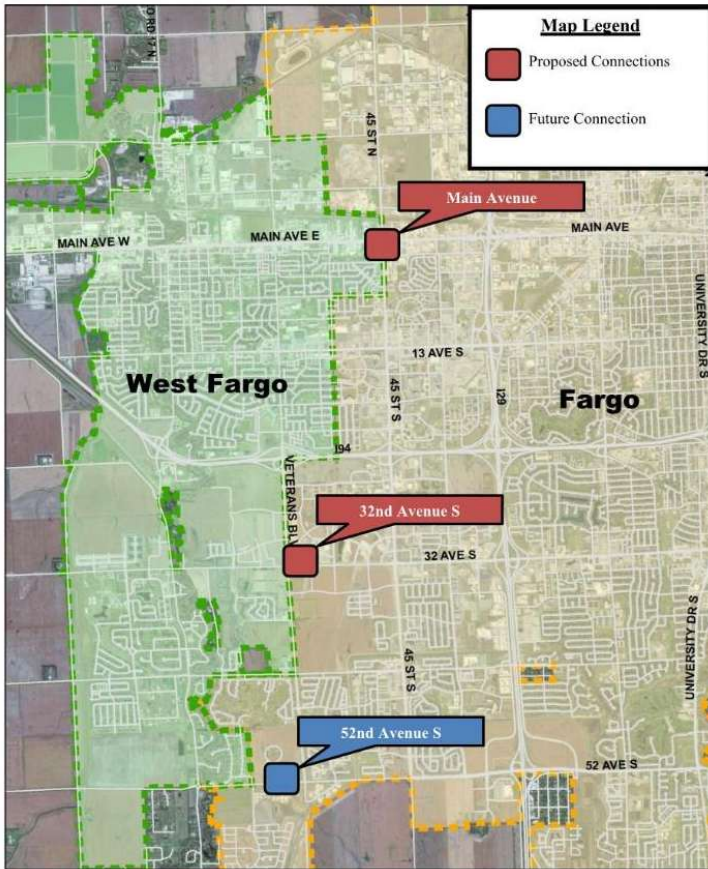
UV Disinfection



# Fargo 15 MGD Integrated Duo Membrane WTP

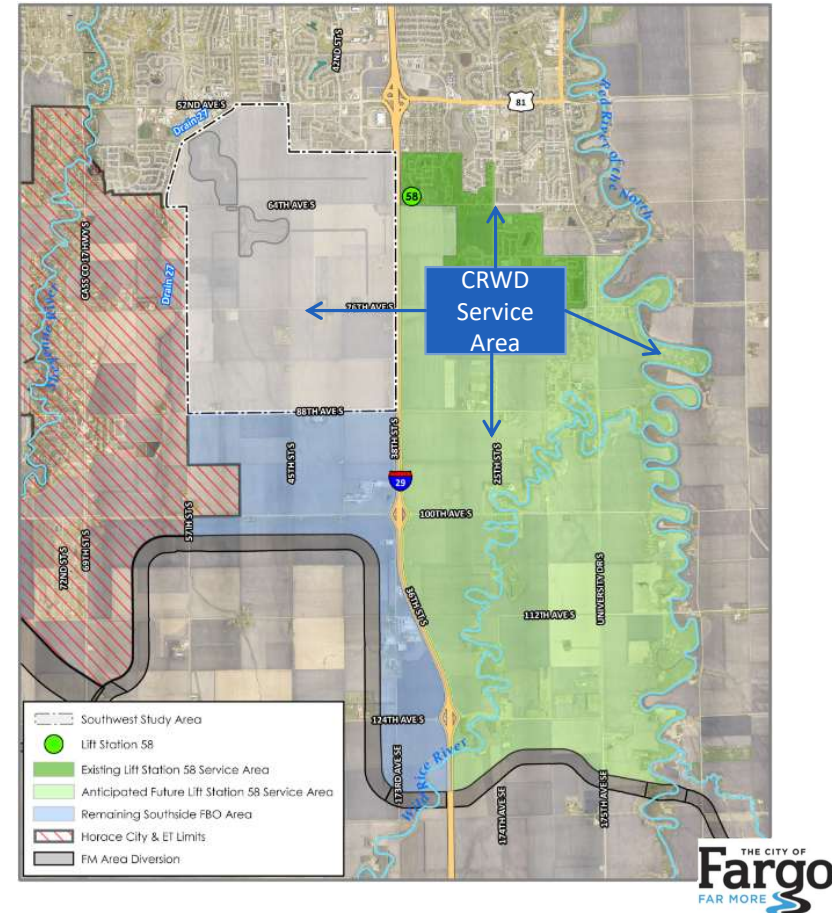


# Regional Water System



**Fargo  
Population  
137,989**

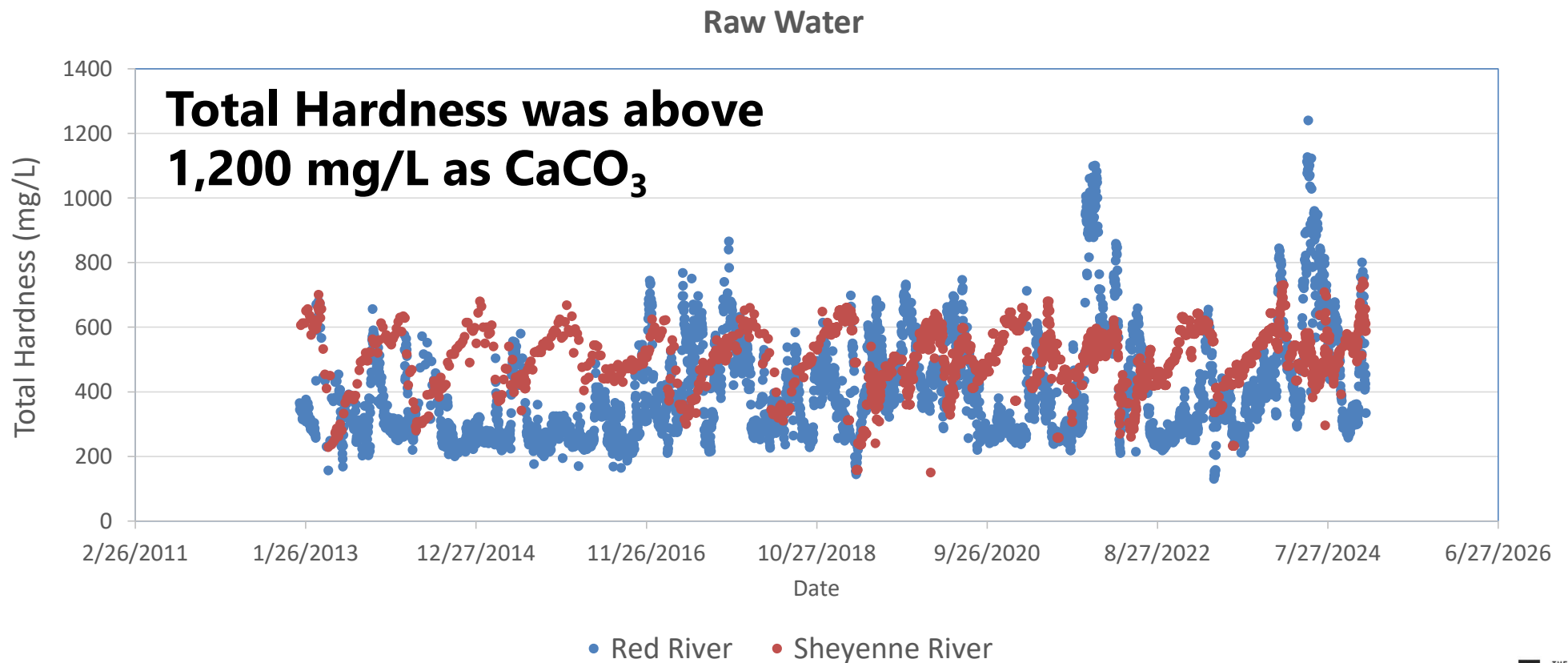
**Regional  
Population  
~200,000**



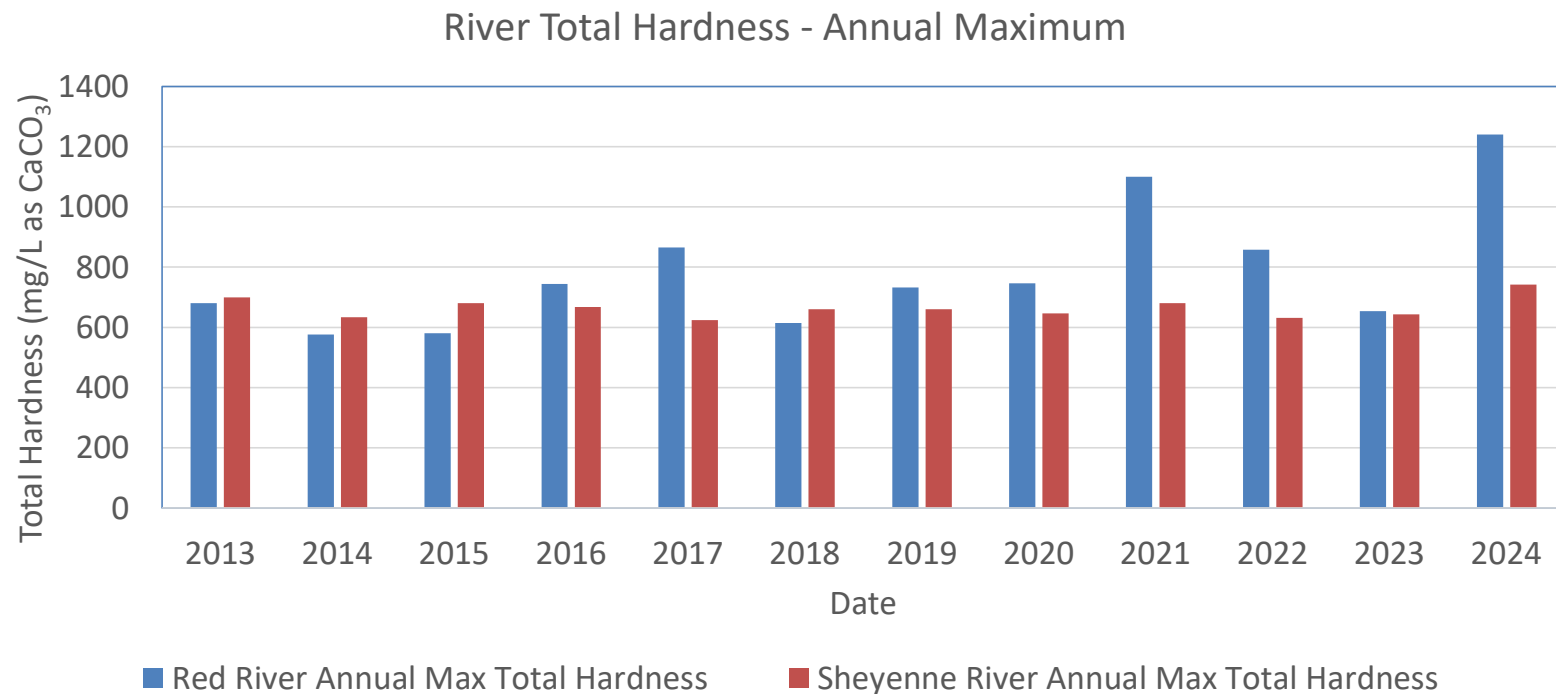


# Fargo Raw Water Overview

# Fargo WTP Raw Water Total Hardness



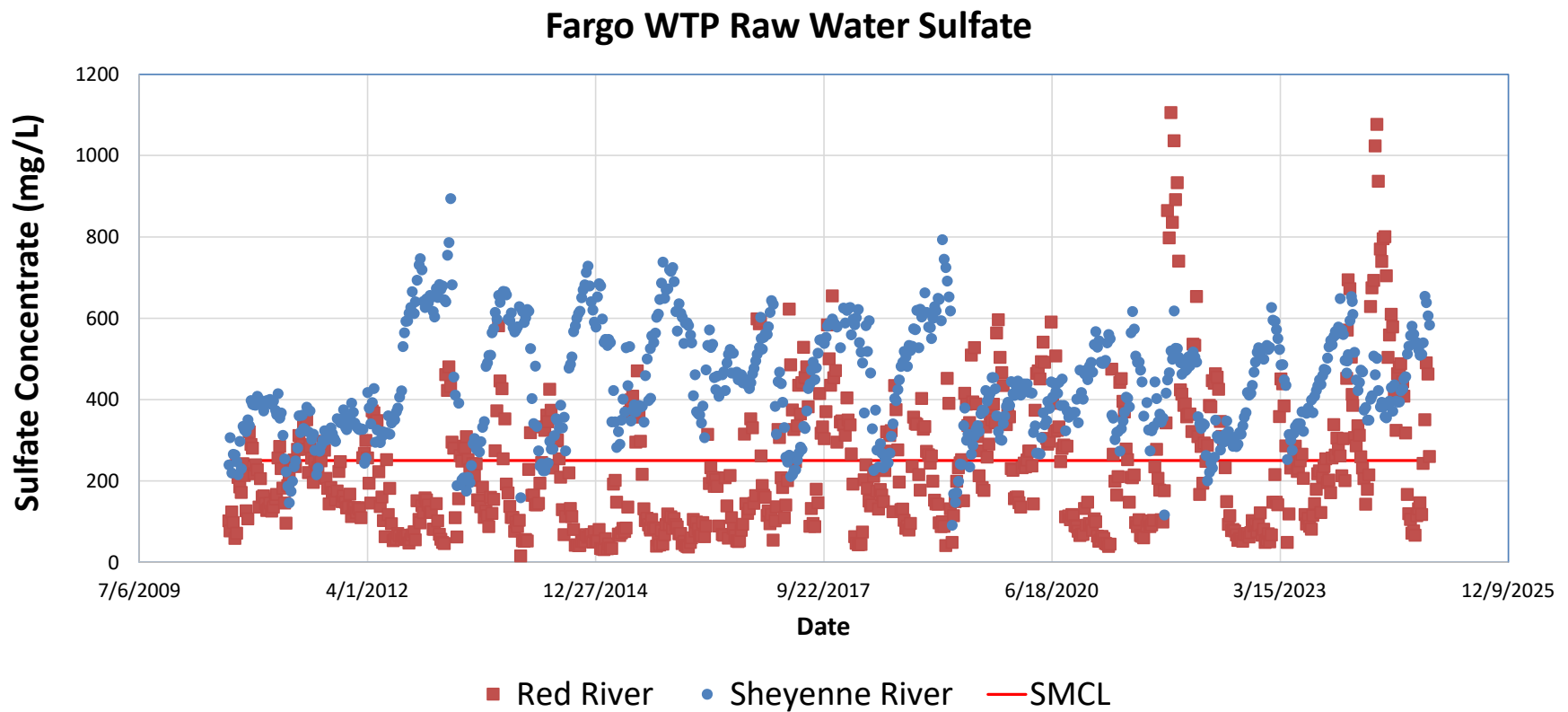
# Fargo WTP Raw Water Total Hardness



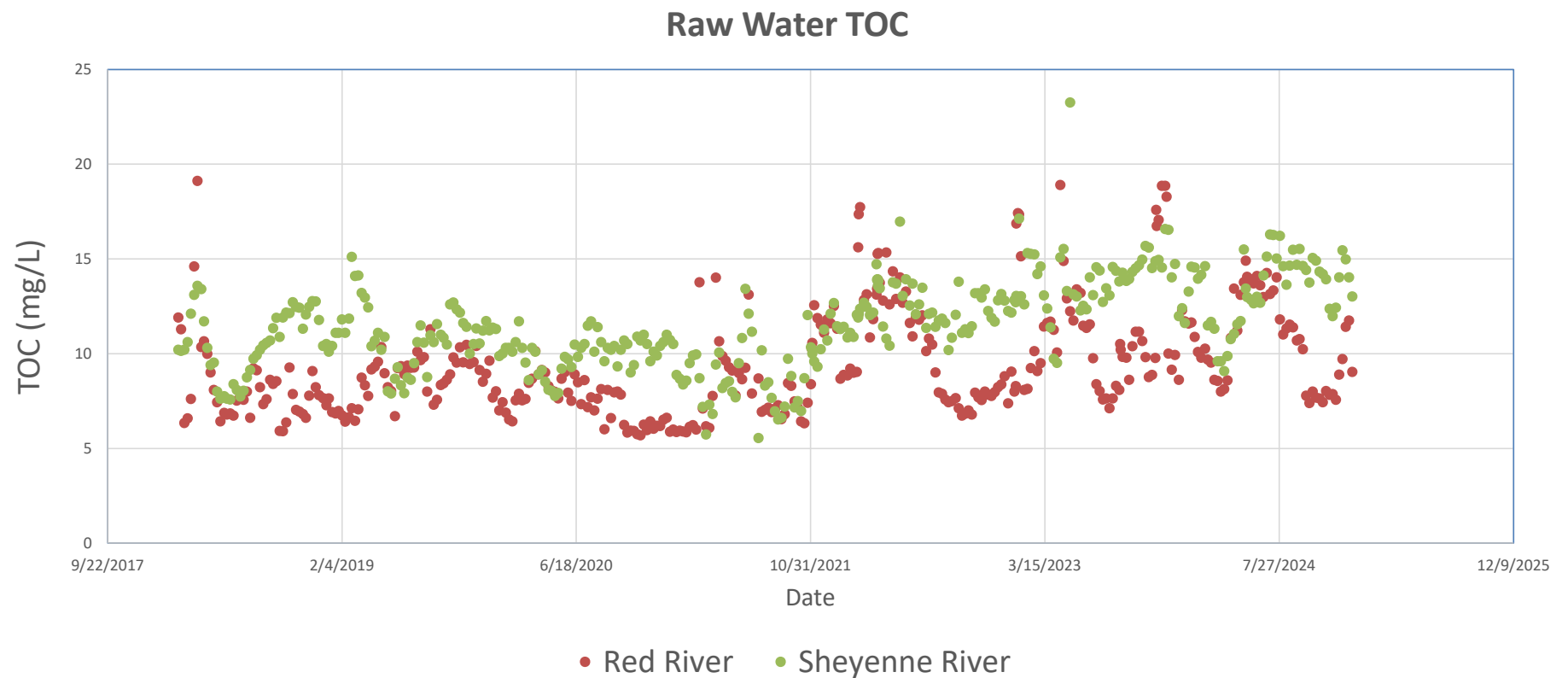
**Rivers are increasingly exhibiting more extreme variations in water quality.**



# Fargo WTP Raw Water - Sulfate



# Fargo WTP Raw Water - TOC



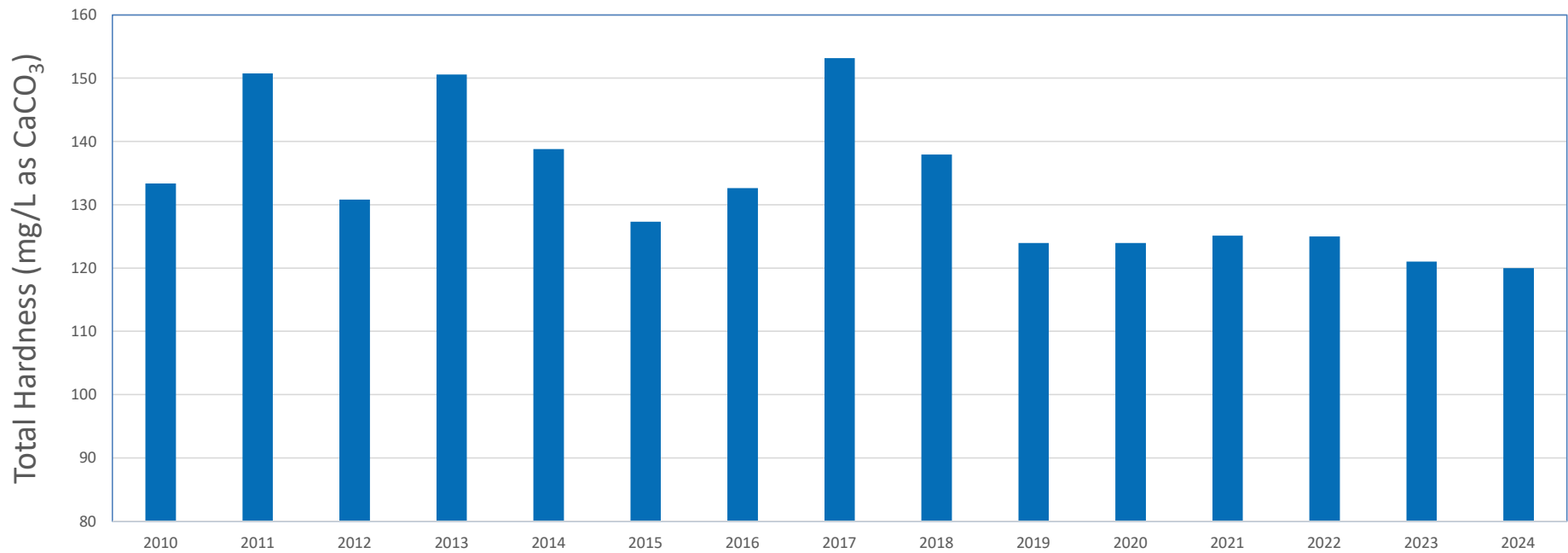
# Fargo WTP Finished Water Goals

- 1 **Meet EPA Primary Drinking Water Standards**
- 2 **Total Hardness: 115-130 (120) mg/L as  $\text{CaCO}_3$**
- 3 **TDS: < 500 mg/L**
- 4 **Sulfate: <250 mg/L**
- 5 **Taste and Odor: no complaints**

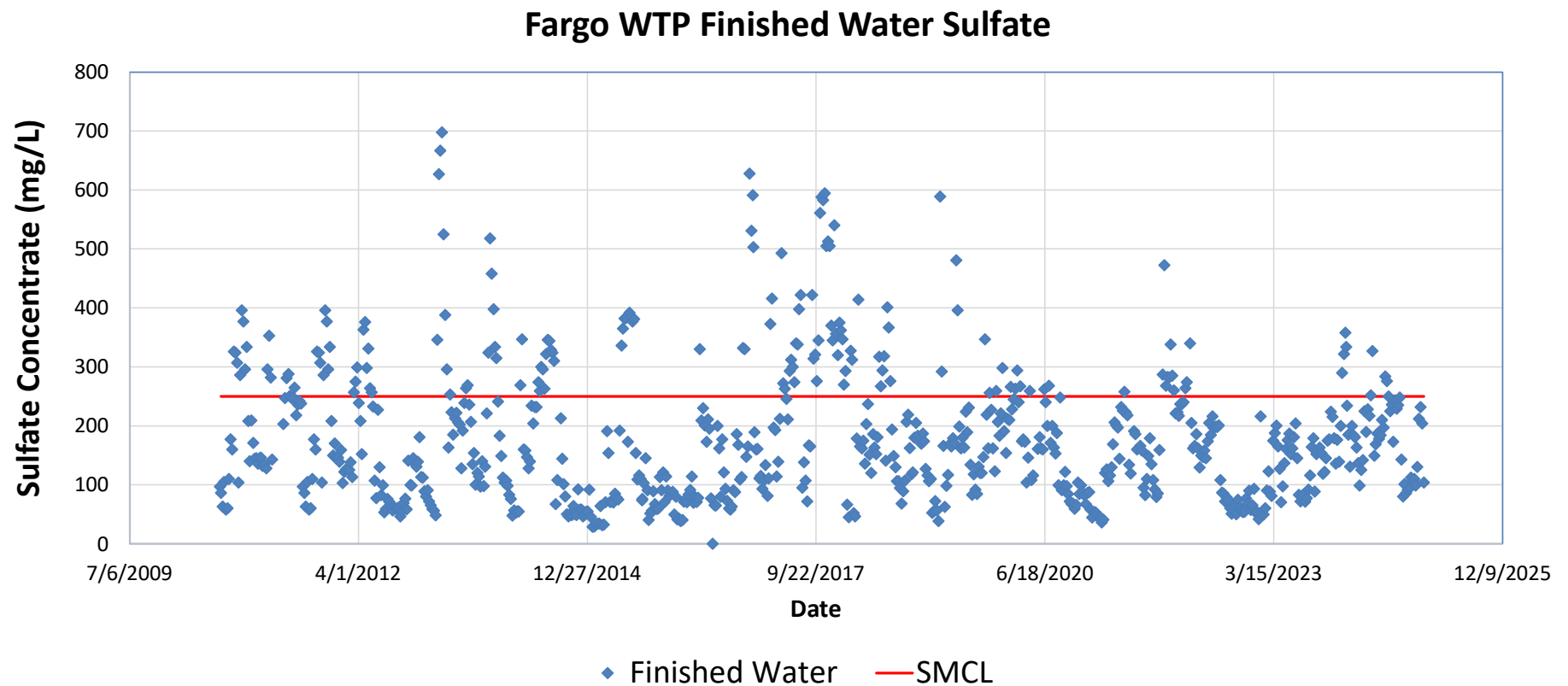


# Fargo WTP Finished Water – Total Hardness

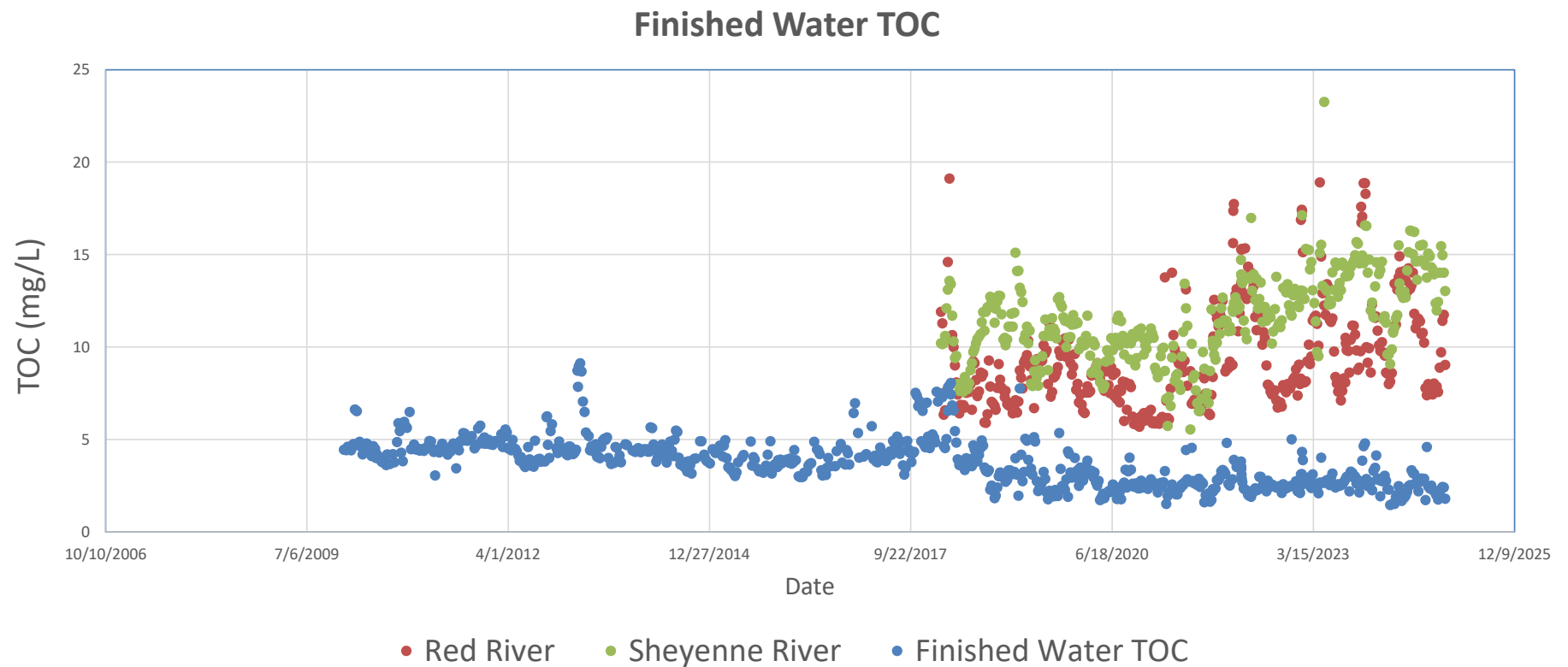
Fargo WTP Finished Water Total Hardness (annual average)



# Fargo WTP Finished Water – Sulfate

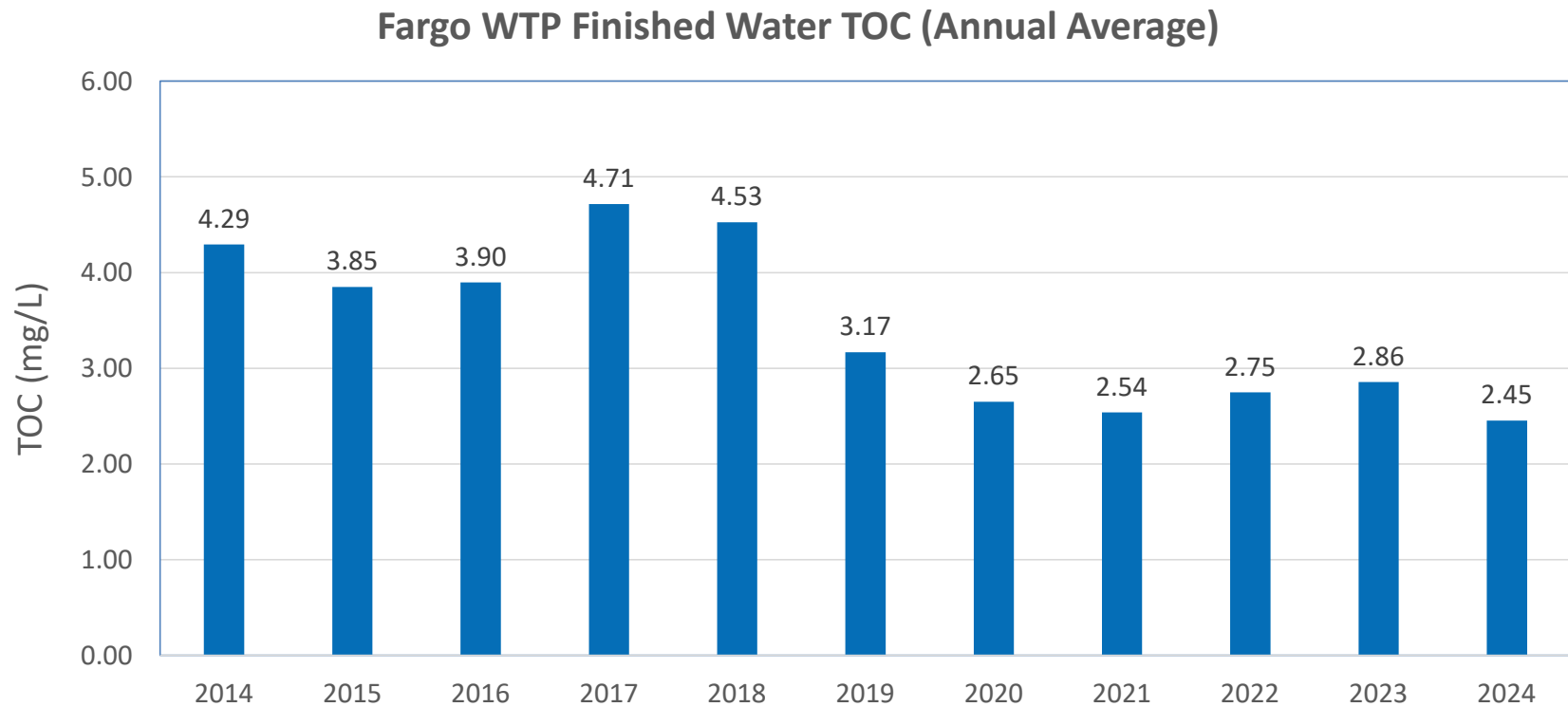


# Finished Water TOC vs Raw Water Natural Organics

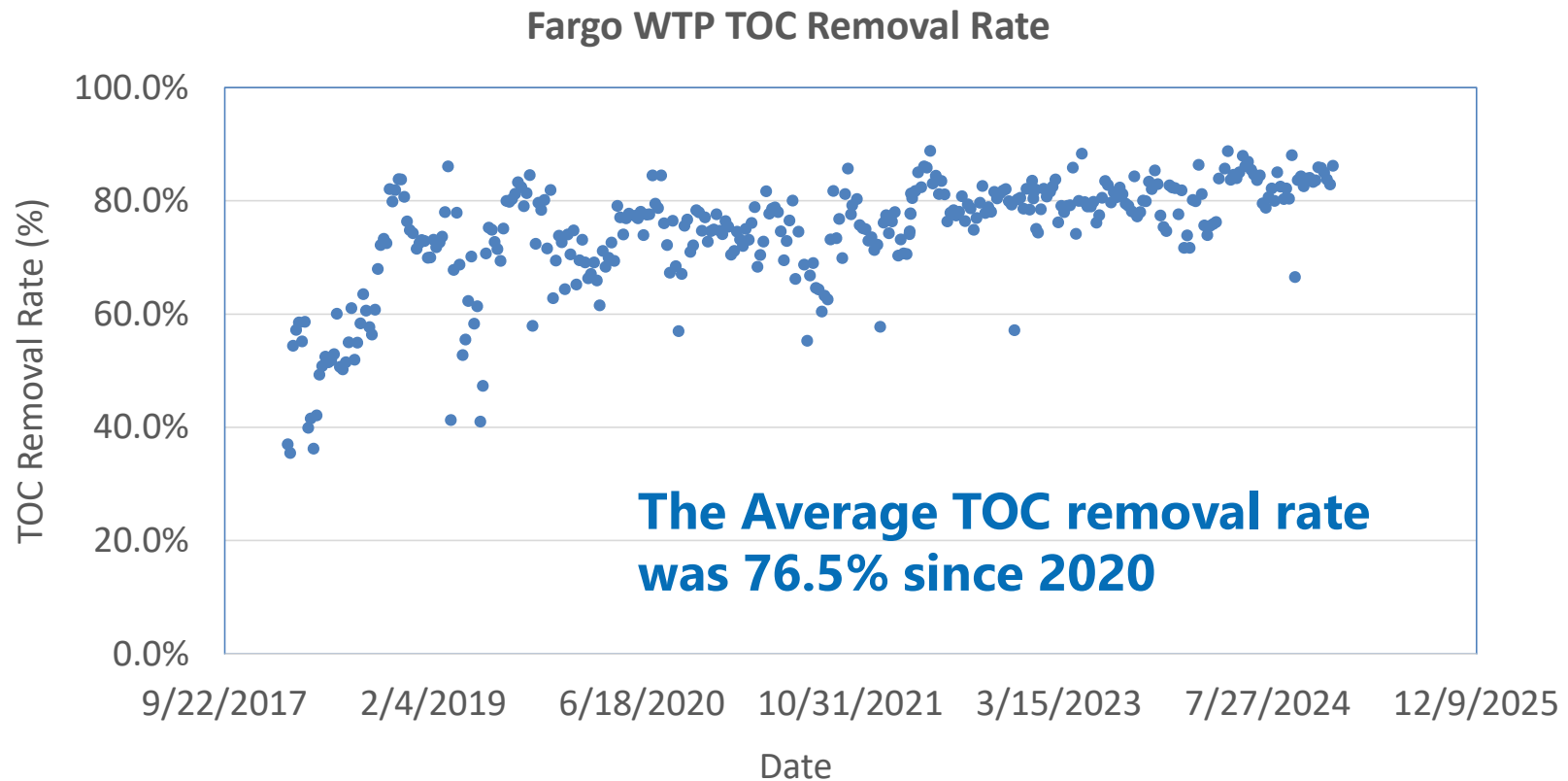




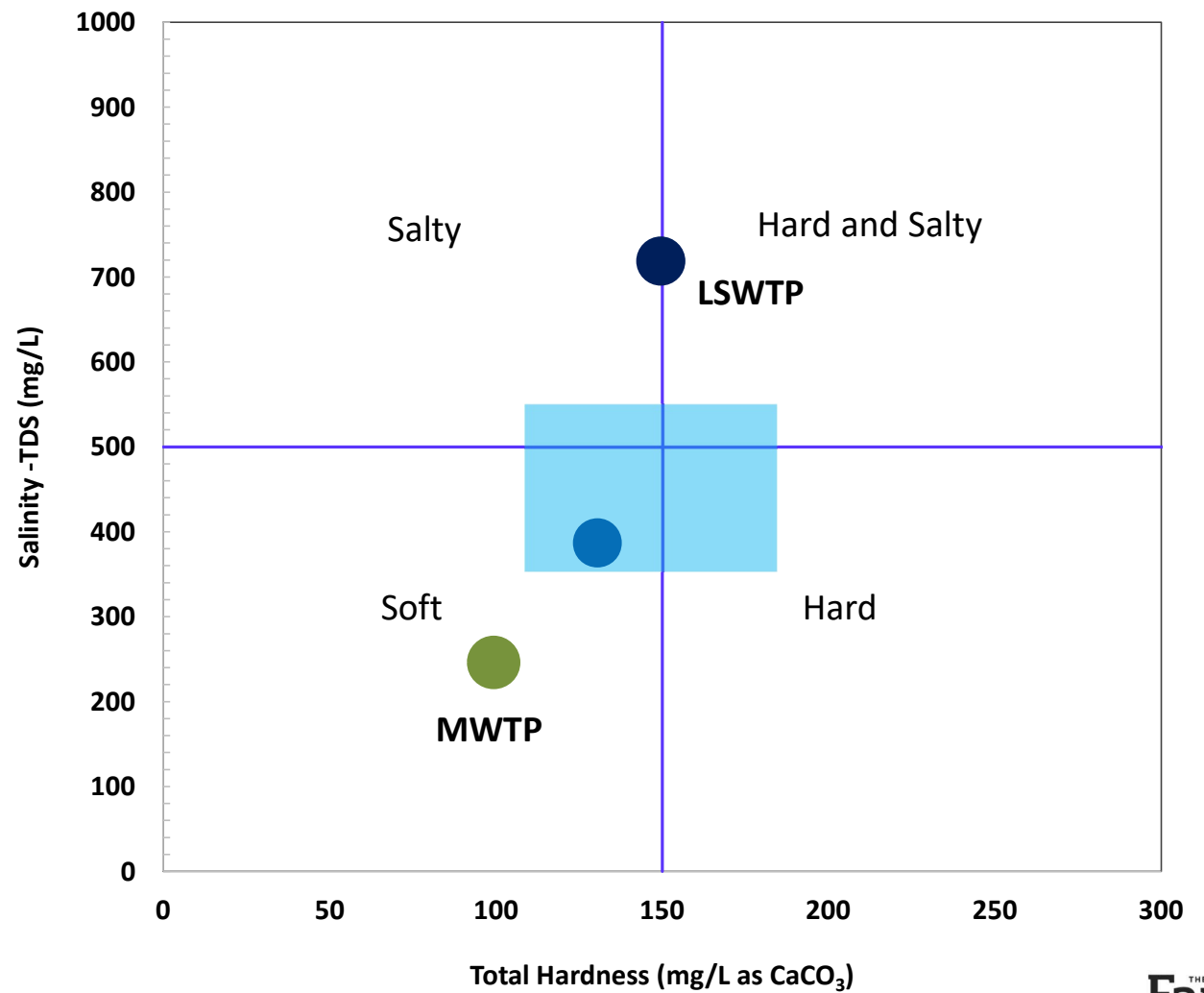
# Finished Water TOC (Annual Average)



# Finished Water TOC (Annual Average)



# Water Quality Quadra



# **Fargo WTP Community Engagement and Recognitions**

# Public Education



**Plant tours to K-12 students, college students, and professionals.**



# TPO. November 2024

Editorial In Fargo: Award for Good Taste. Reputation for Quality.

## In Fargo: Award for Good Taste. Reputation for Quality.

The North Dakota city of Fargo turned to membrane filtration to deal with significant changes and variability in source water

Appeared in print as "Tastes Great. Best Filtered."

By James Careless

December 2024

Top Performer - Plant



Jessey Pederson, left, membrane plant specialist, and Dan Portlock, water utility engineer, in the treatment plant's lobby.

Want tap water that tastes really great? Then go to Fargo.

For two years in a row, 2022 and 2023, the output from the Fargo Water Treatment Plant was named the Best Tasting in the state at the North Dakota Water & Pollution Control Conference. To date, Fargo is the only city to...



<https://www.tpomag.com/editorial/2024/12/in-fargo-award-for-good-taste-reputation-for-quality>

# Top-Tier Operation Staff

## AMTA and AWWA announce awardees at the Membrane Technology Conference & Exposition

📅 February 25, 2022

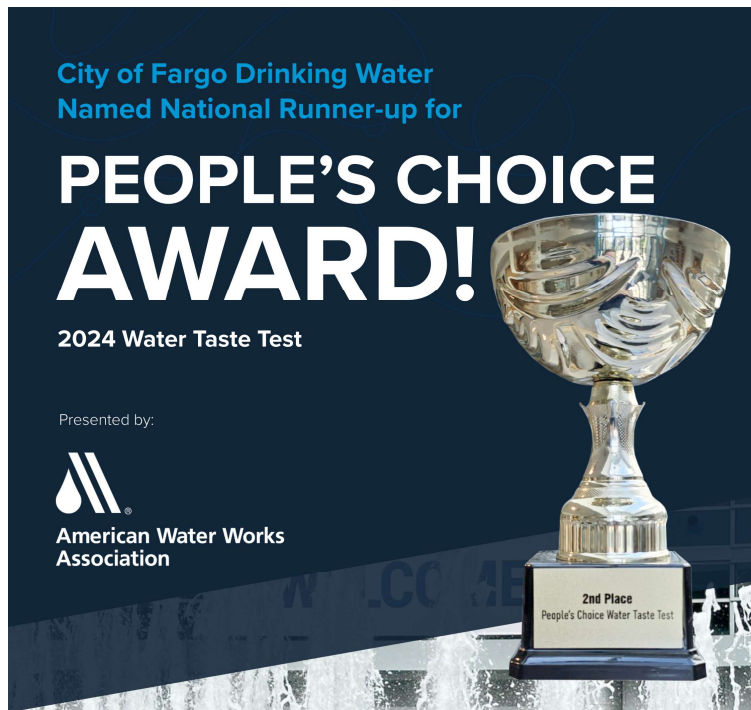
[Press Releases](#)

The [American Membrane Technology Association](#) (AMTA) and the [American Water Works Association](#) (AWWA) announced awardees at the 2022 Membrane Technology Conference & Exposition (MTC) in Las Vegas.

**Brian Ward of the City of Fargo Water Treatment Plant in Fargo, N.D.**, was presented with this year's Robert O. Vernon Operator of the Year Award. The award recognizes outstanding contributions by a plant operator working at a membrane filtration, desalination or water reuse facility that resulted in significant, long-term improvement in water production and/or water reuse.



# We Care About Water Quality





# 2024 Membrane Facility of the Year Award



# **Impossible Triangle**

Quality, Efficiency, Cost

The background is a solid blue color. A thick black diagonal line starts from the bottom left and extends towards the top right, creating a triangular shape on the right side of the slide.

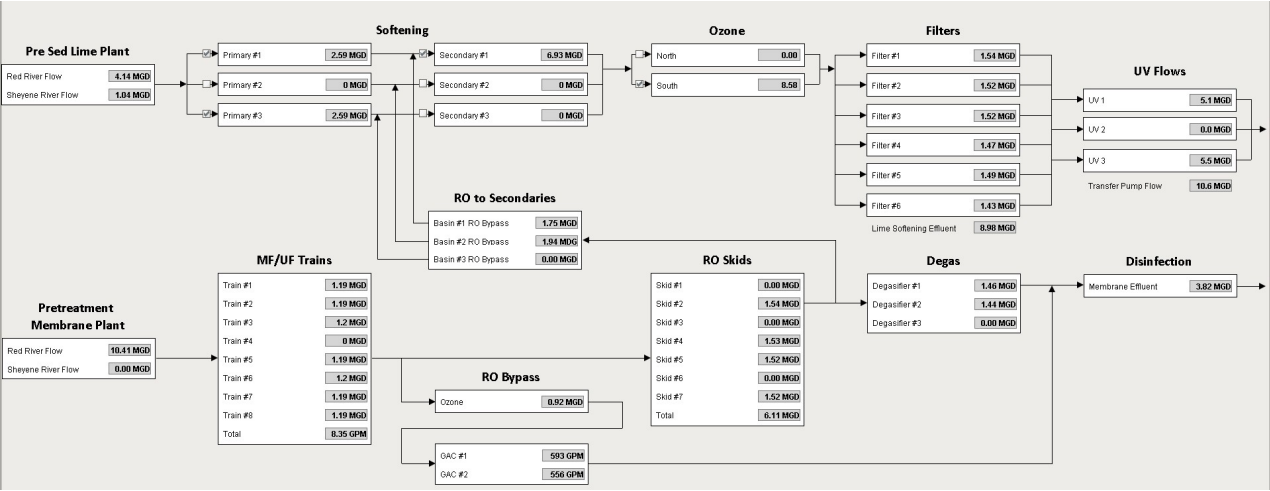
# Win Them All



**How to operate two plants  
in a way to achieve:**

- 1 Great Water Quality**
- 2 High Efficiency**
- 3 Low Cost**

# Operation Strategies



Operation Scenarios

| Scenario No. | LSWTP |          | MWTP |          | RO Transfer |
|--------------|-------|----------|------|----------|-------------|
|              | RED   | Sheyenne | RED  | Sheyenne |             |
| 1            | X     |          | X    |          |             |
| 2            | X     |          | X    |          | X           |
| 3            | X     |          |      | X        |             |
| 4            | X     |          |      | X        | X           |
| 5            |       | X        | X    |          |             |
| 6            |       | X        | X    |          | X           |
| 7            |       | X        |      | X        |             |
| 8            |       | X        |      | X        | X           |
| 9            | X     | X        | X    |          |             |
| 10           | X     | X        | X    |          | X           |
| 11           | X     | X        |      | X        |             |
| 12           | X     | X        |      | X        | X           |
| 13           | X     | X        | X    | X        |             |
| 14           | X     | X        | X    | X        | X           |





# Operation Strategies

## **Operation variables:**

1. Raw water selection: two rivers
2. Flow split between two WTPs
3. Intermediate RO permeate transfer between two WTPs
4. Finished water quality from each plant
5. 13 chemicals

**Production Cost Model: A real time chemical cost estimate based upon real-time water quality monitoring**

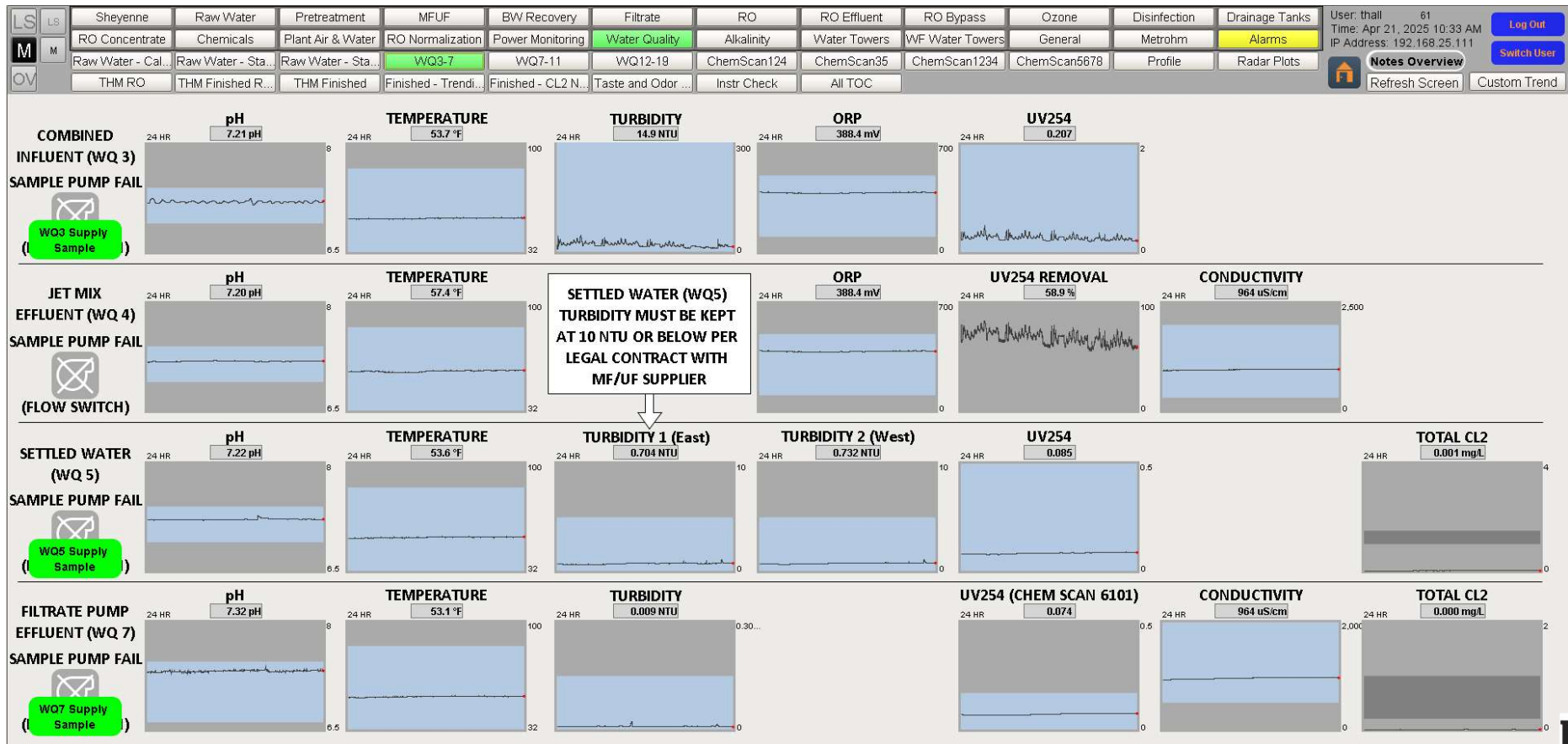
# Team Approaches

**Fargo WTP has been working closely with NDDEQ, ND PFA, and DWR on various projects aimed at improving finished water quality and enhancing overall plant efficiency.**



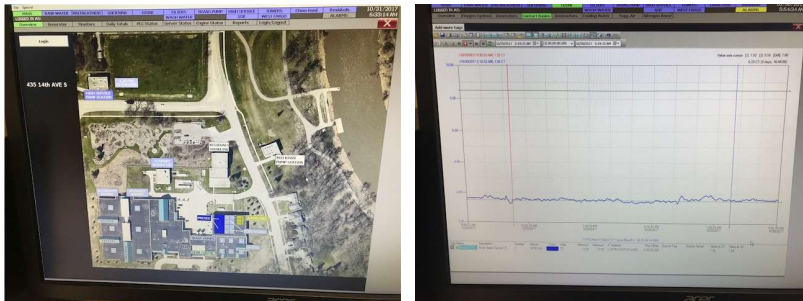
# Tools in Place for Operational Improvement

## A New SCADA System



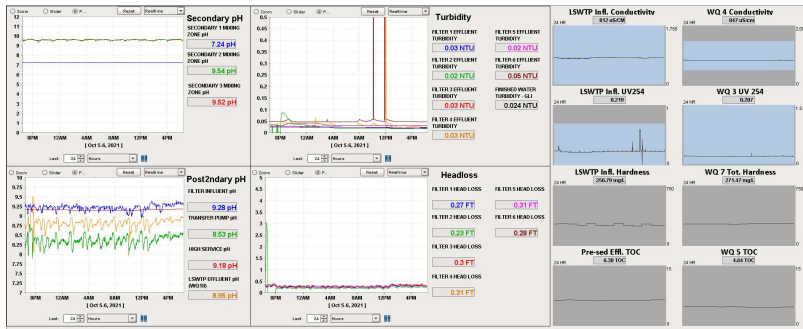
# Information Speed with New SCADA System

## Over 100x Faster for Operations Personnel



### Past Fargo WTP SCADA System

- 4 mouse clicks to get trend of single data point
- Slight data Retrieval delay
- **Data point not trended with other related data**
- Limited performance 'information'

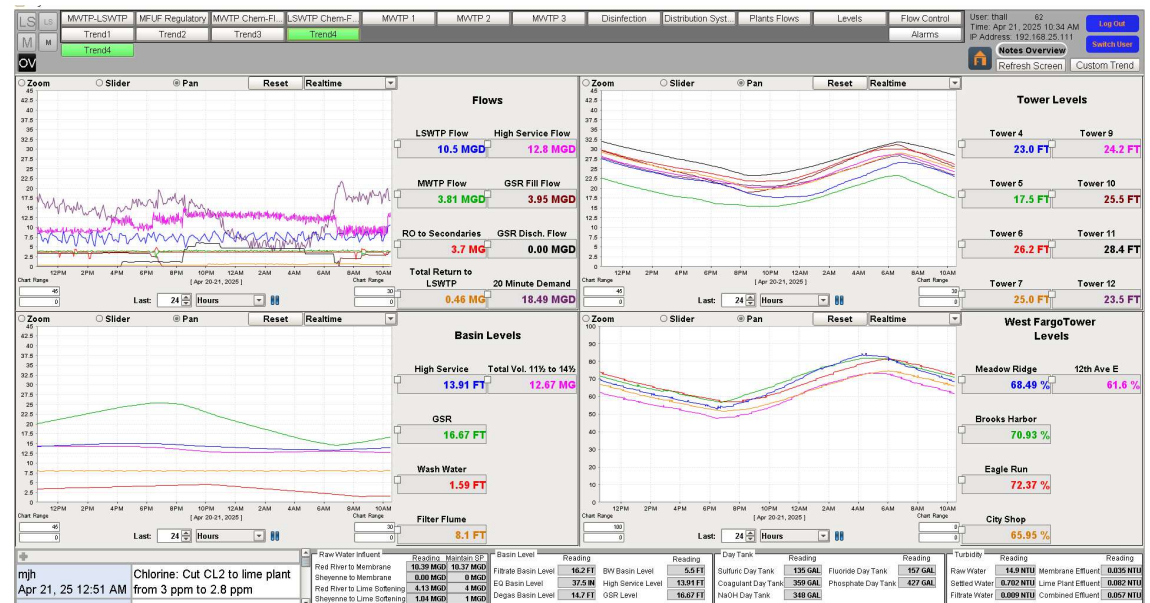


### New Fargo WTP SCADA System

- Each mouse click 4 to 6 different trend graphics
- Multiple related data point on each screen
- Graphic load quickly (minimum delay)
- **Example screen has 27 trended data points**
- **4 mouse clicks get roughly 108 data points trended**

Times about 15 end users → 1,500 times faster plant-wide!

# Full WTP Assessment in Seconds to Minutes





# Tools in Place for Operational Improvement

## Chemical Cost Calculator

LS

LS

M

M

Ov

Sheyenne

Raw Water

Pretreatment

MFUF

BW Recovery

Filtrate

RO

RO Effluent

RO Bypass

Ozone

Disinfection

Drainage Tanks

RO Concentrate

Chemicals

Plant Air & Water

RO Normalization

Power Monitoring

Water Quality

Alkalinity

Water Towers

WVF Water Towers

General

Metrohm

Alarms

Ambient Gas

Sulfuric-PACL-Bi...

Citric-Anti-H2O2

Fluoride-Phosph...

Sodium Hydroxide

Copper Sulfate

Dosing

Transfer

Chlorine

Ammonia

Digital Alarms

Level and Press...

Cost Calculations

User: thall 1

Time: Apr 17, 2025 01:01 PM

IP Address: 192.168.25.111

Log Out

Switch User

Notes Overview

Refresh Screen

Custom Trend

| Chemical Name         | Chemical Pump Tag Name | Description                          | Feed Point         | Chemical Cost (\$ / lb) | Dosage    | \$ / Day | \$ / 1,000 Finished | Calculated Flow | Calculated Dosage | Calculated \$ / Day | Calculated \$ / 1,000 | Cost/Day Difference | Cost/1,000 Difference |
|-----------------------|------------------------|--------------------------------------|--------------------|-------------------------|-----------|----------|---------------------|-----------------|-------------------|---------------------|-----------------------|---------------------|-----------------------|
| PACI                  | 16_CMP_2103            | COAGULANT METERING PUMP NO. 1        | Coagulant-PACL     | \$0.28                  | 55 PPM    | 0 \$     | 0.00 \$             |                 | 35 mg/L           | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| PACI                  | 16_CMP_2203            | COAGULANT METERING PUMP NO. 2        | Coagulant-PACL     | \$0.28                  | 55 PPM    | 2,438 \$ | 0.18 \$             |                 | 35 mg/L           | 825 \$              | 0.16 \$               | -1,613 \$           | -0.02 \$              |
| Sulfuric Acid -93%    | 16_CMP_1103            | SULFURIC ACID METERING PUMP NO. 1    | Sulfuric Acid 1    | \$0.1023                | 34.68 PPM | 562 \$   | 0.04 \$             |                 | 22.42 mg/L        | 193 \$              | 0.04 \$               | -368 \$             | 0.00 \$               |
| Sulfuric Acid -93%    | 16_CMP_1203            | SULFURIC ACID METERING PUMP NO. 2    | Sulfuric Acid 1    | \$0.1023                | 34.68 PPM | 0 \$     | 0.00 \$             |                 | 22.42 mg/L        | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Sulfuric Acid -93%    | 16_CMP_1303            | SULFURIC ACID METERING PUMP NO. 3    | Sulfuric Acid 1    | \$0.1023                | 34.68 PPM | 0 \$     | 0.00 \$             |                 | 22.42 mg/L        | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Pretreatment Totals   |                        |                                      |                    |                         |           | 3,002 \$ | 0.22 \$             | 10.1 MGD        |                   | 1,019 \$            | 0.20 \$               | -1,983 \$           | -0.02 \$              |
| Anti-scalant          | 16_CMP_4103            | ANTISCALANT METERING PUMP NO. 1      | Antiscalant        | \$3.35                  | 2 PPM     | 0 \$     | 0.00 \$             |                 | 1.48 mg/L         | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Anti-scalant          | 16_CMP_4203            | ANTISCALANT METERING PUMP NO. 2      | Antiscalant        | \$3.35                  | 2 PPM     | 660 \$   | 0.05 \$             |                 | 1.48 mg/L         | 254 \$              | 0.05 \$               | -406 \$             | 0.00 \$               |
| Antiscalant/RO Totals |                        |                                      |                    |                         |           | 660 \$   | 0.05 \$             | 6.13 MGD        |                   | 254 \$              | 0.05 \$               | -406 \$             | 0.00 \$               |
| Fluoride              | 15_CMP_6103            | FLUORIDE METERING PUMP NO. 1         | Fluoride           | \$0.22                  | 0.65 PPM  | 16 \$    | 0.00 \$             |                 | 0.7 mg/L          | 7 \$                | 0.00 \$               | -10 \$              | 0.00 \$               |
| Fluoride              | 15_CMP_6203            | FLUORIDE METERING PUMP NO. 2         | Fluoride           | \$0.22                  | 0.65 PPM  | 0 \$     | 0.00 \$             |                 | 0.7 mg/L          | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Phosphate             | 15_CMP_7103            | PHOSPHATE METERING PUMP NO. 1        | Phosphate          | \$1.13                  | 0.5 PPM   | 0 \$     | 0.00 \$             |                 | 0.5 mg/L          | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Phosphate             | 15_CMP_7203            | PHOSPHATE METERING PUMP NO. 2        | Phosphate          | \$1.13                  | 2.5 PPM   | 319 \$   | 0.00 \$             |                 | 2.3 mg/L          | 111 \$              | 0.02 \$               | -207 \$             | -0.02 \$              |
| Phosphate 1 Totals    |                        |                                      |                    |                         |           | 319 \$   | 0.00 \$             |                 |                   | 111 \$              | 0.02 \$               | -207 \$             | -0.02 \$              |
| Sodium Hydroxide      | 16_CMP_3103            | SODIUM HYDROXIDE METERING PUMP NO. 1 | Sodium Hydroxide 1 | \$0.1985                | 16.67 PPM | 0 \$     | 0.00 \$             |                 | 0 mg/L            | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Sodium Hydroxide      | 16_CMP_3203            | SODIUM HYDROXIDE METERING PUMP NO. 2 | Sodium Hydroxide 1 | \$0.1985                | 16.67 PPM | 373 \$   | 0.03 \$             |                 | 0 mg/L            | 0 \$                | 0.00 \$               | -373 \$             | -0.03 \$              |
| Chlorine              | CF_4XX                 | CHLORINE FEEDER SELECTED             | Chlorine 2         | \$0.2685                | 3.75 mg/L | 114 \$   | 0.00 \$             |                 | 3.5 mg/L          | 40 \$               | 0.01 \$               | -73 \$              | -0.01 \$              |
| Chlorine              | CF_4XX                 | CHLORINE FEEDER SELECTED             | Chlorine 3         | \$0.2685                | 0 mg/L    | 0 \$     | 0.00 \$             |                 | 0 mg/L            | 0 \$                | 0.00 \$               | 0 \$                | 0.00 \$               |
| Chlorine Totals       |                        |                                      |                    |                         |           | 114 \$   | 0.00 \$             |                 |                   | 40 \$               | 0.01 \$               | -73 \$              | -0.01 \$              |
| Ammonia               | AM_CF_4XX              | AMMONIA FEEDER SELECTED              | Ammonia 3          | \$2.06                  | 1.05 mg/L | 244 \$   | 0.00 \$             |                 | 1.01 mg/L         | 89 \$               | 0.02 \$               | -154 \$             | -0.02 \$              |
| Ammonia Totals        |                        |                                      |                    |                         |           | 244 \$   | 0.00 \$             |                 |                   | 89 \$               | 0.02 \$               | -154 \$             | -0.02 \$              |
| Finished Totals       |                        |                                      |                    |                         |           | 1,066 \$ | 0.03 \$             | 5.13 MGD        |                   | 247 \$              | 0.05 \$               | -818 \$             | -0.02 \$              |
| Plant Chemical Totals |                        |                                      |                    |                         |           | 4,728 \$ | 0.30 \$             |                 |                   | 1,520 \$            | 0.30 \$               | -3,207 \$           | 0.00 \$               |
| Plant Power Totals    |                        |                                      |                    |                         |           | 1,263 \$ | 0.09 \$             |                 |                   |                     |                       |                     |                       |
| Plant Combined Totals |                        |                                      |                    |                         |           | 5,987 \$ | 0.39 \$             |                 |                   |                     |                       |                     |                       |

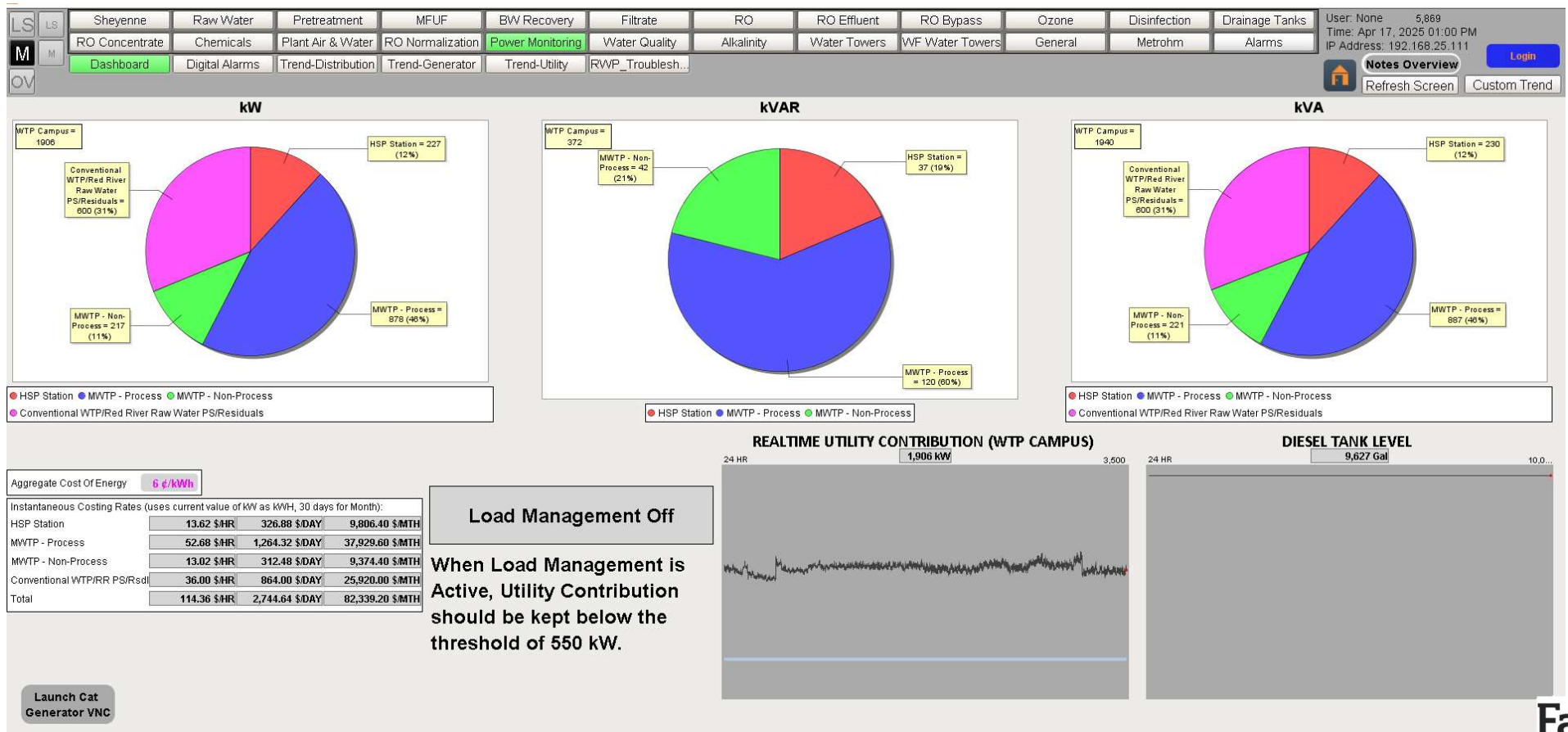
Cost/30-Day Difference

-96,129 \$

Cost/Year Difference

# Tools in Place for Operational Improvement

## Power Cost Analysis

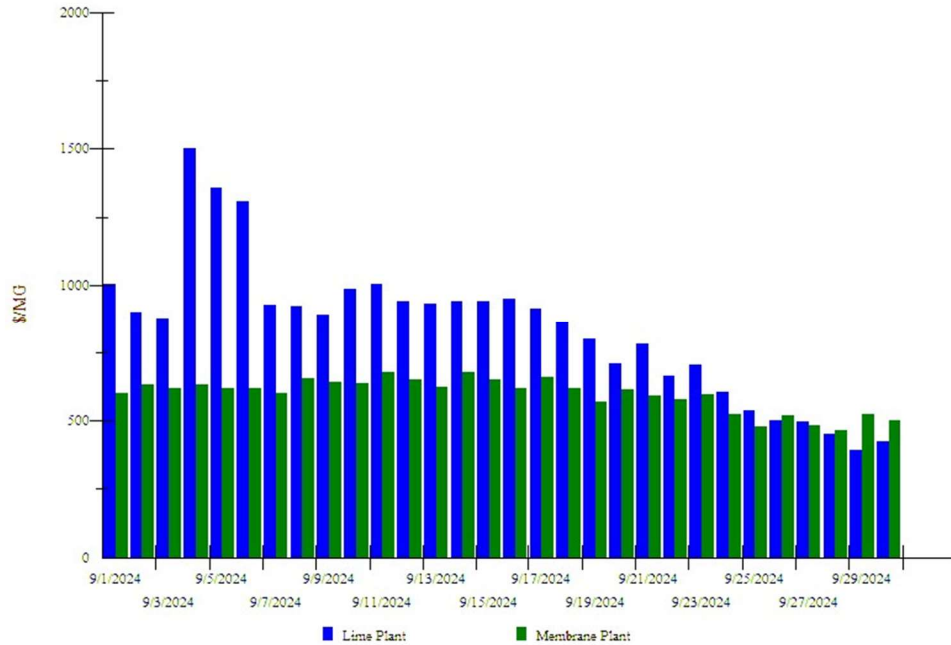




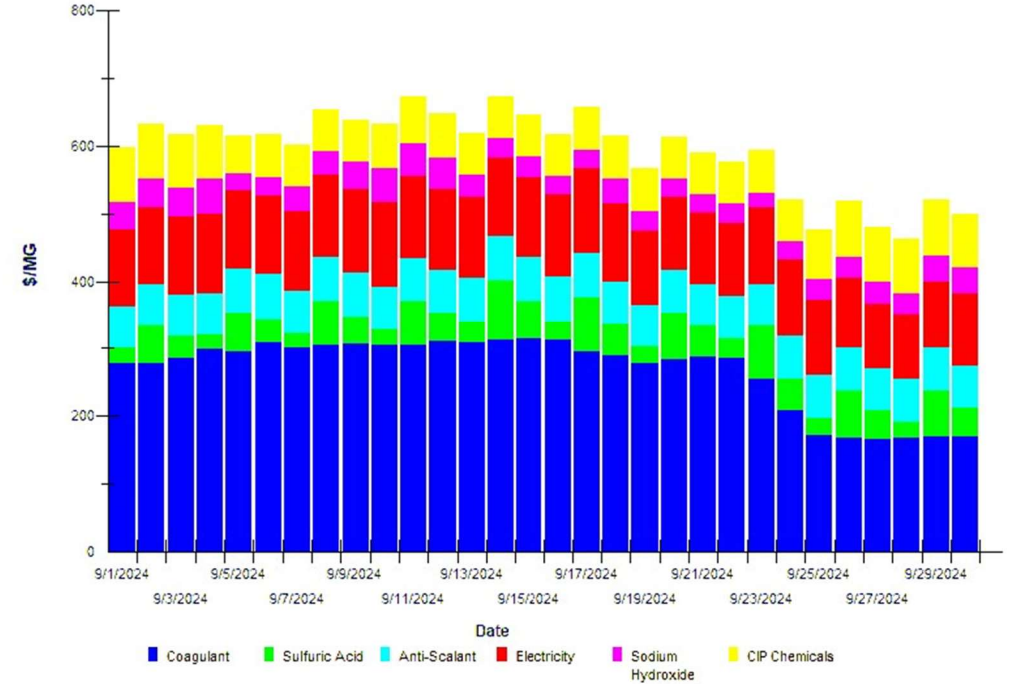
# Tools in Place for Operational Improvement

## Treatment Cost Model

Primary costs per Million Gallons



Membrane Plant Primary Costs per Million Gallons

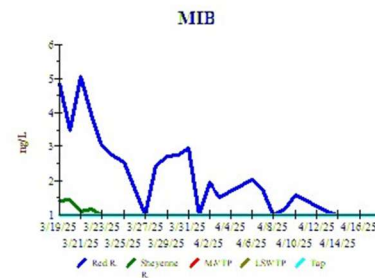
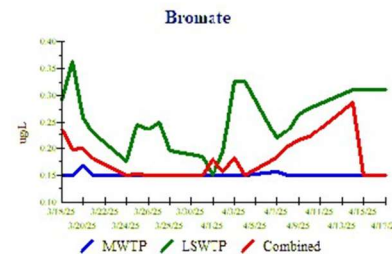
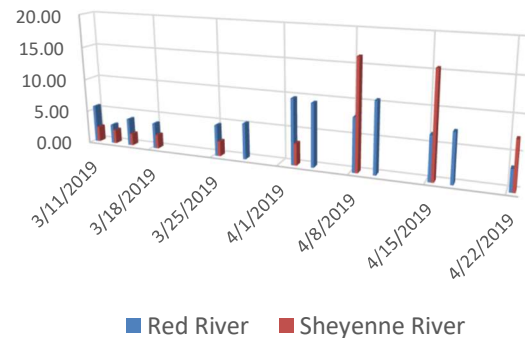


# Tools in Place for Operational Improvement

## Environmental Lab



Raw Water Geosmin Concentrations  
(Taste & Odor Causing)



|         | WQ13<br>Bromate | WQ 18<br>Bromate | WQ 19<br>Bromate | Red<br>River<br>Geosmin | Shey.<br>River<br>Geosmin | WQ 13<br>Geosmin | WQ 18<br>Geosmin | Tap<br>Geosmin | Red<br>River<br>MIB | Shey.<br>River<br>MIB | WQ 13<br>MIB | WQ 18<br>MIB | Tap<br>MIB |
|---------|-----------------|------------------|------------------|-------------------------|---------------------------|------------------|------------------|----------------|---------------------|-----------------------|--------------|--------------|------------|
|         | ug/L            | ug/L             | ug/L             | PPT                     | PPT                       | PPT              | PPT              | PPT            | PPT                 | PPT                   | PPT          | PPT          | PPT        |
| 3/18/25 | <0.150          | 0.292            | 0.236            | 6.025                   | 3.558                     | <1.000           | <1.000           | <1.000         | 4.845               | 1.393                 | <1.000       | <1.000       | <1.000     |
| 3/19/25 | <0.150          | 0.364            | 0.198            | 3.439                   | 2.982                     | <1.000           | <1.000           | <1.000         | 3.504               | 1.446                 | <1.000       | <1.000       | <1.000     |
| 3/20/25 | 0.168           | 0.259            | 0.199            | 5.183                   | 3.040                     | <1.000           | <1.000           | <1.000         | 5.071               | 1.088                 | <1.000       | <1.000       | <1.000     |
| 3/21/25 | <0.150          | 0.229            | 0.181            | 5.055                   | 2.907                     | <1.000           | <1.000           | <1.000         | 3.963               | 1.155                 | <1.000       | <1.000       | <1.000     |
| 3/22/25 |                 |                  |                  | 2.821                   | <1.000                    | <1.000           | <1.000           | <1.000         | 3.030               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/23/25 |                 |                  |                  | 2.065                   | 1.150                     | <1.000           | <1.000           | <1.000         | 2.728               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/24/25 | <0.150          | 0.176            | <0.150           | 4.522                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.549               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/25/25 | <0.150          | 0.245            | 0.152            |                         |                           |                  |                  |                |                     |                       |              |              |            |
| 3/26/25 | <0.150          | 0.236            | <0.150           | <1.000                  | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/27/25 | <0.150          | 0.250            | <0.150           | 2.382                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.433               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/28/25 | <0.150          | 0.196            | <0.150           | 3.567                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.719               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/29/25 |                 |                  |                  | 2.944                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.759               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/30/25 |                 |                  |                  | 2.901                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.934               | <1.000                | <1.000       | <1.000       | <1.000     |
| 3/31/25 | <0.150          | 0.185            | <0.150           | <1.000                  | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/1/25  | <0.150          | <0.150           | 0.180            | 2.154                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.938               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/2/25  | <0.150          | 0.194            | 0.157            | 1.688                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.501               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/3/25  | <0.150          | 0.327            | 0.183            |                         |                           |                  |                  |                |                     |                       |              |              |            |
| 4/4/25  | <0.150          | 0.327            | <0.150           |                         |                           |                  |                  |                |                     |                       |              |              |            |
| 4/5/25  |                 |                  |                  | 2.526                   | <1.000                    | <1.000           | <1.000           | <1.000         | 2.010               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/6/25  |                 |                  |                  | 2.489                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.750               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/7/25  | 0.156           | 0.219            | 0.182            | 1.056                   | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/8/25  | <0.150          | 0.235            | 0.205            | 1.289                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.168               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/9/25  | <0.150          | 0.266            | 0.216            | 1.948                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.577               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/10/25 | <0.150          | 0.277            | 0.221            |                         |                           |                  |                  |                |                     |                       |              |              |            |
| 4/11/25 |                 |                  |                  |                         |                           |                  |                  |                |                     |                       |              |              |            |
| 4/12/25 |                 |                  |                  | 1.886                   | <1.000                    | <1.000           | <1.000           | <1.000         | 1.104               | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/13/25 |                 |                  |                  | 1.830                   | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/14/25 | <0.150          | 0.311            | 0.288            | <1.000                  | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/15/25 | <0.150          |                  | <0.150           | 1.003                   | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/16/25 | <0.150          |                  | <0.150           | 1.464                   | <1.000                    | <1.000           | <1.000           | <1.000         | <1.000              | <1.000                | <1.000       | <1.000       | <1.000     |
| 4/17/25 | <0.150          |                  | <0.150           |                         |                           |                  |                  |                |                     |                       |              |              |            |

# Tools in Place for Operational Improvement

## Treatment Cost Model

FileHomeInsertPage LayoutFormulasDataReviewViewHelpTell me what you want to do

CutCopyFormat Painter

Arial16A<sup>+</sup>A<sup>-</sup>

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General

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Conditional Formatting

Format as Table

Normal

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Calculation

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Explanatory...

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Delete

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Clear

Sort & Find & Filter

Find & Select

Editing

A1

fx

Jar Tests

|    | A                 | B      | C       | D                 | E       | F       | G            | H       | I | J | K | L | M | N | O | P | Q | R | S | T | U |
|----|-------------------|--------|---------|-------------------|---------|---------|--------------|---------|---|---|---|---|---|---|---|---|---|---|---|---|---|
| 1  | Jar Tests         |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 2  | PACL density      |        | 1.343   | DADMAC density    |         | 1.051   | Jar size (L) | 2.0     |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 3  | Stock sol. (mg/L) |        | 20,000  | Stock sol. (mg/L) |         | 20,000  | Starting DOC |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 4  | PACL price/lb     |        | \$0.485 | DADMAC price/lb   |         | \$1.490 |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 5  |                   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 6  | Jar:              |        | 1       | 2                 | 3       | 4       | 5            | 6       |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 7  | ratio             | PACL   | 80%     | 80%               | 80%     | 90%     | 90%          | 90%     |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 8  |                   | DADMAC | 20%     | 20%               | 20%     | 10%     | 10%          | 10%     |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 9  | dose (mg/L)       | total  | 1       | 2                 | 3       | 1       | 2            | 3       |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 10 |                   | PACL   |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 11 |                   | DADMAC |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 12 | vol. (µl) per Jar | PACL   | 80      | 160               | 240     | 90      | 180          | 270     |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 13 |                   | DADMAC | 40      | 80                | 120     | 20      | 40           | 60      |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 14 | Turbidity (NTU)   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 15 | DOC (mg/L)        |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 16 | DOC removal (%)   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 17 | price/MG          |        | \$8.21  | \$16.41           | \$24.62 | \$6.13  | \$12.25      | \$18.38 |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 18 |                   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 19 |                   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |
| 20 |                   |        |         |                   |         |         |              |         |   |   |   |   |   |   |   |   |   |   |   |   |   |

Jar doses

| Calculated dosages |     |     |     |     |     |  |
|--------------------|-----|-----|-----|-----|-----|--|
| 1                  | 2   | 3   | 4   | 5   | 6   |  |
| 80%                | 80% | 80% | 90% | 90% | 90% |  |
| 20%                | 20% | 20% | 10% | 10% | 10% |  |
| 1                  | 2   | 3   | 1   | 2   | 3   |  |
| 0.8                | 1.6 | 2.4 | 0.9 | 1.8 | 2.7 |  |
| 0.4                | 0.8 | 1.2 | 0.2 | 0.4 | 0.6 |  |

# Tools in Place for Operational Improvement

## Treatment Cost Model

Membrane plant flow planner - Excel

FileHomeInsertPage LayoutFormulasDataReviewViewHelpTell me what you want to do

CutCopyFormat Painter

ClipboardFont

Alignment

Number

Styles

Cells

Editing

Calibri11

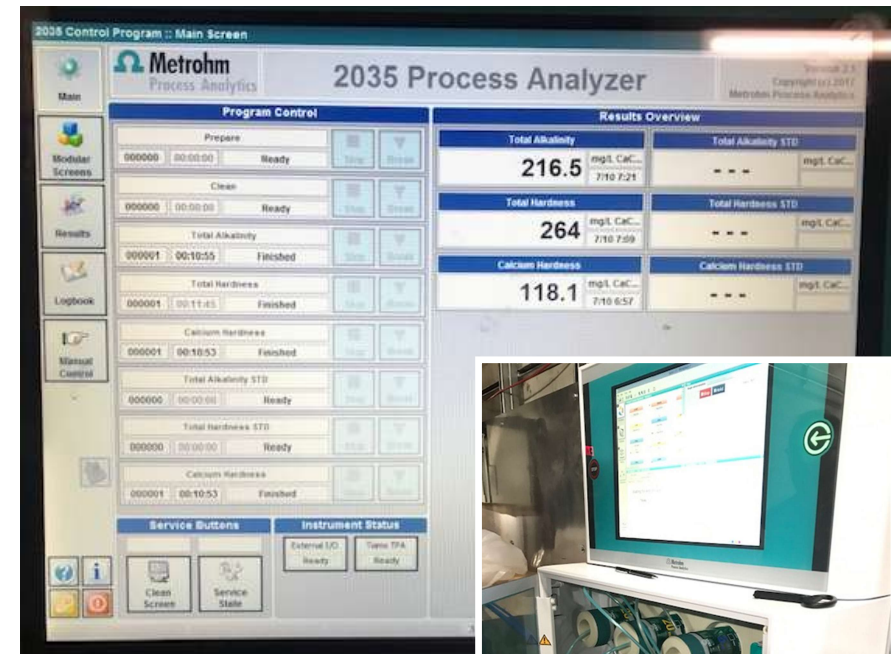
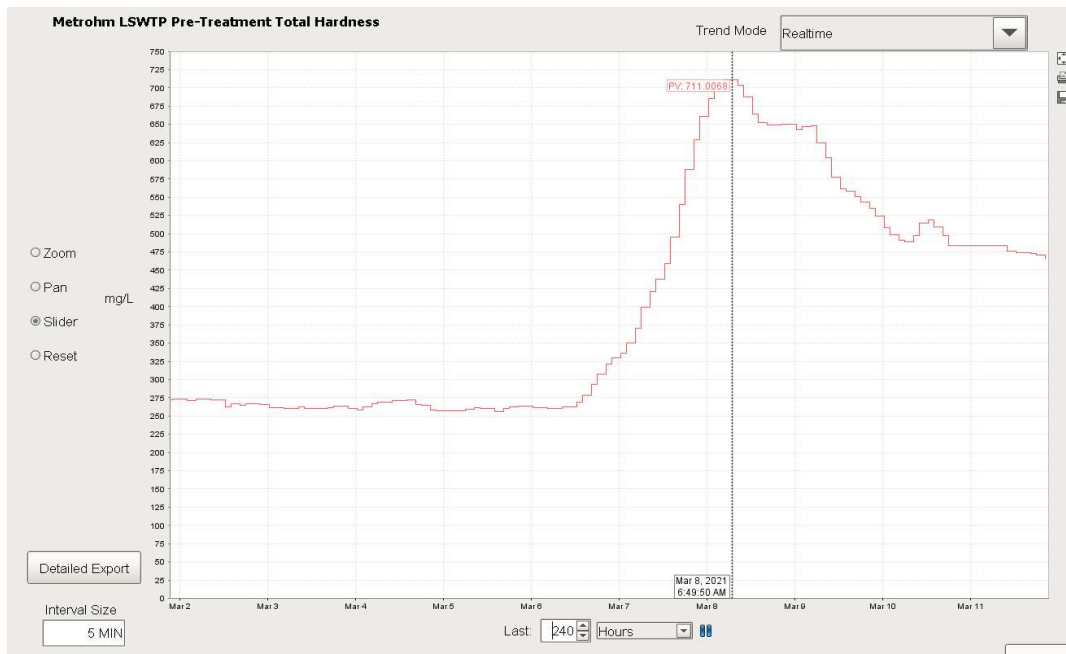
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# Tools in Place for Operational Improvement

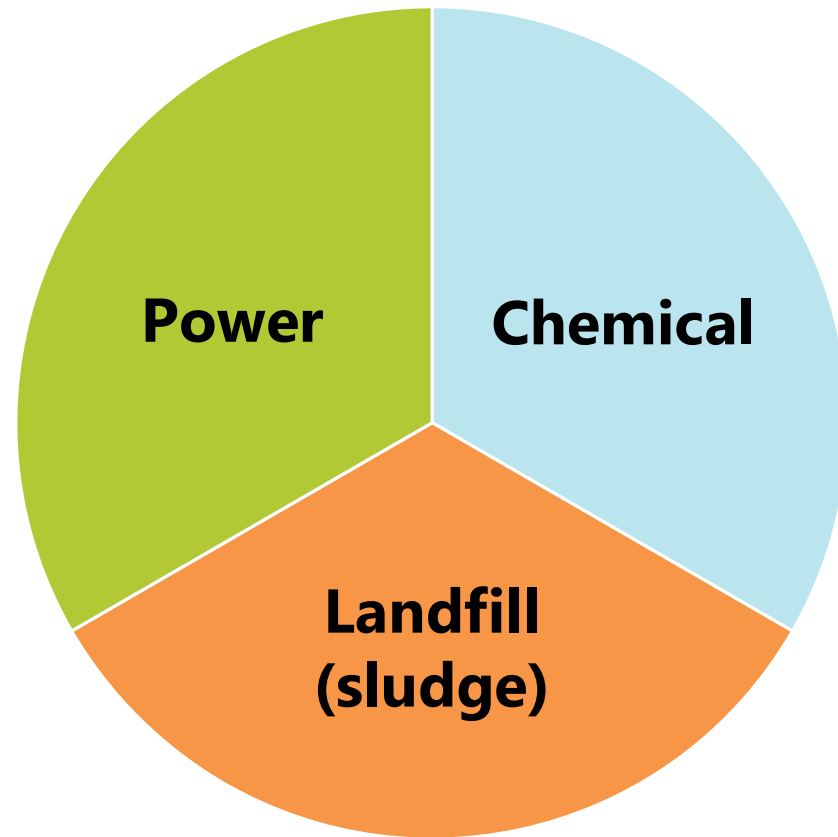
## Continuous Monitoring



**Accurate Cost to Produce  
Water at Each Plant and  
Finished Water Quality from  
Each Plant are Key to Achieve  
the Impossible Triangle**

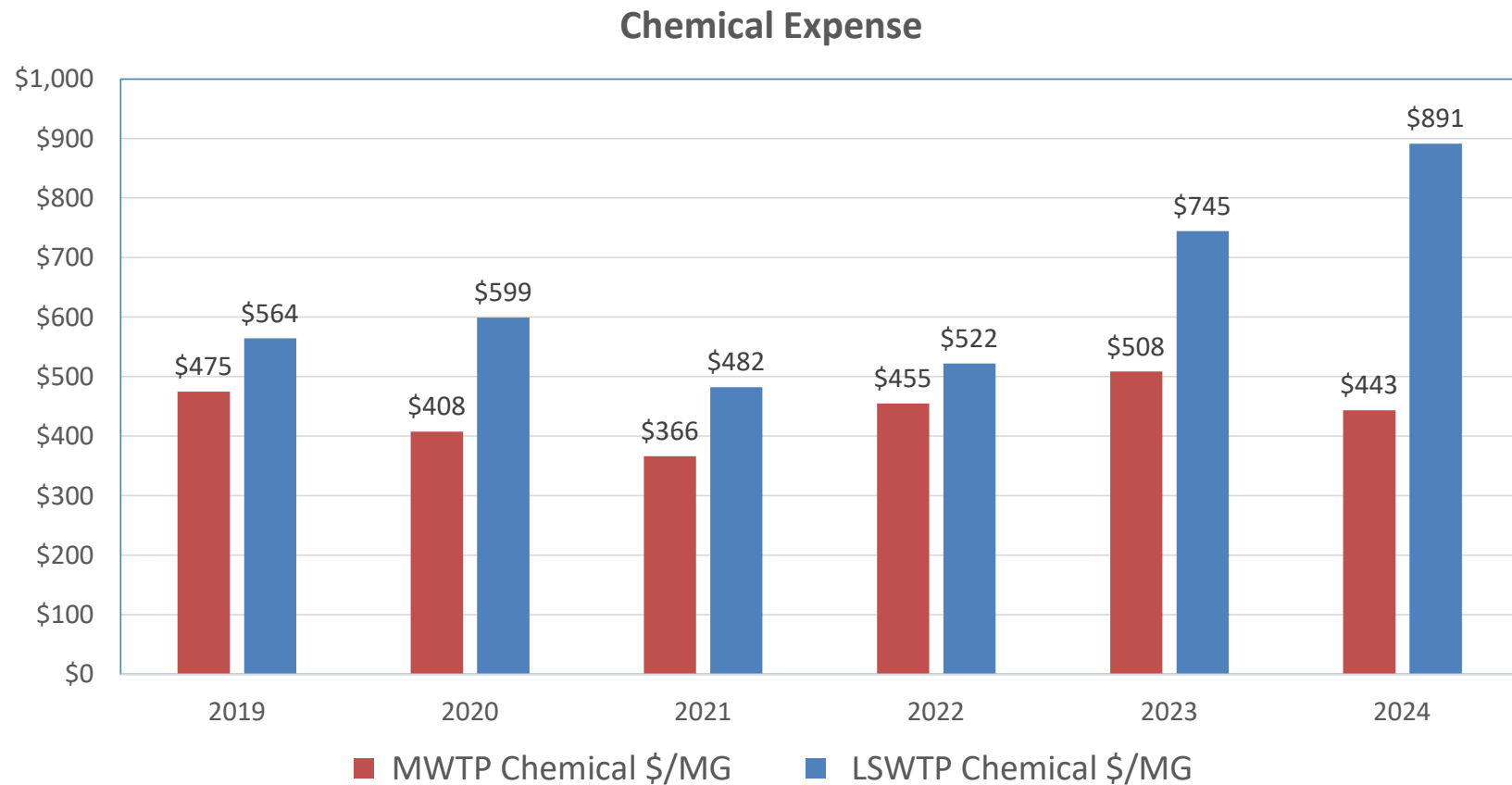
# Major Cost to Produce Water

## Big Three



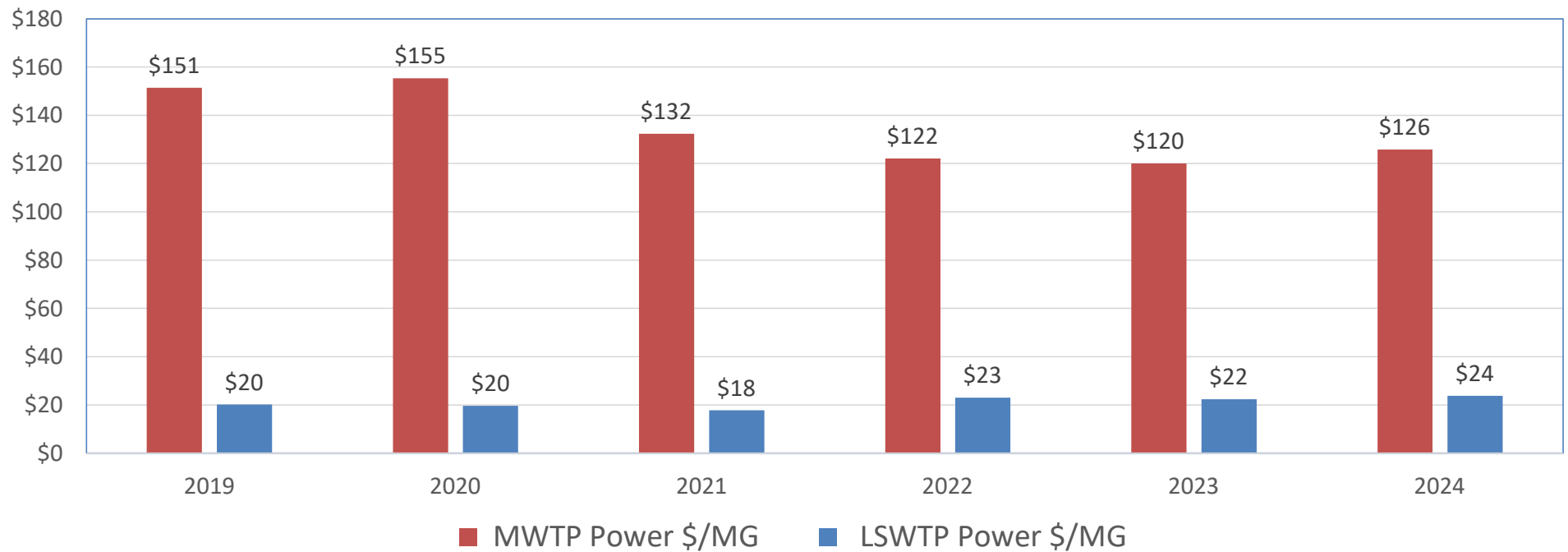


# Chemical Cost



# Power Cost

Power Expense

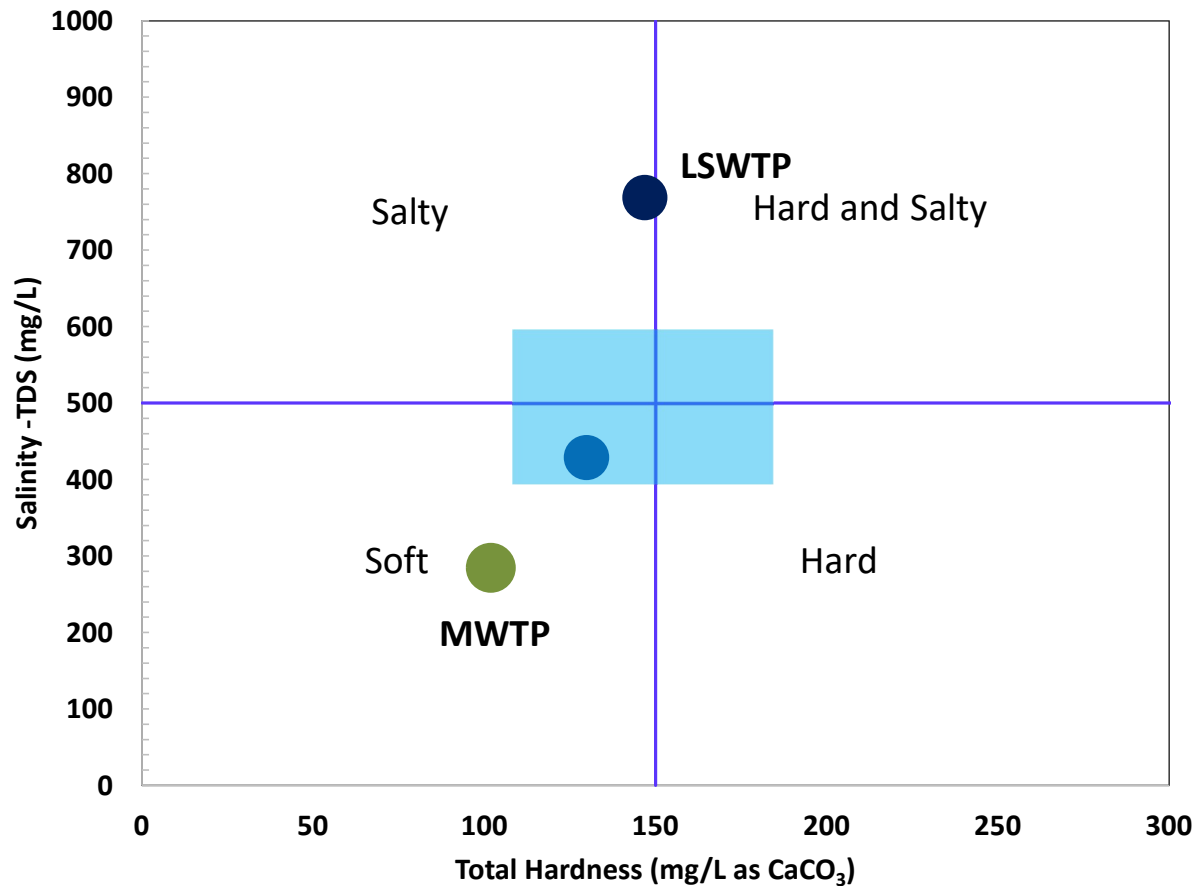


# Cost to Produce Water

## Chemical + Power Expense

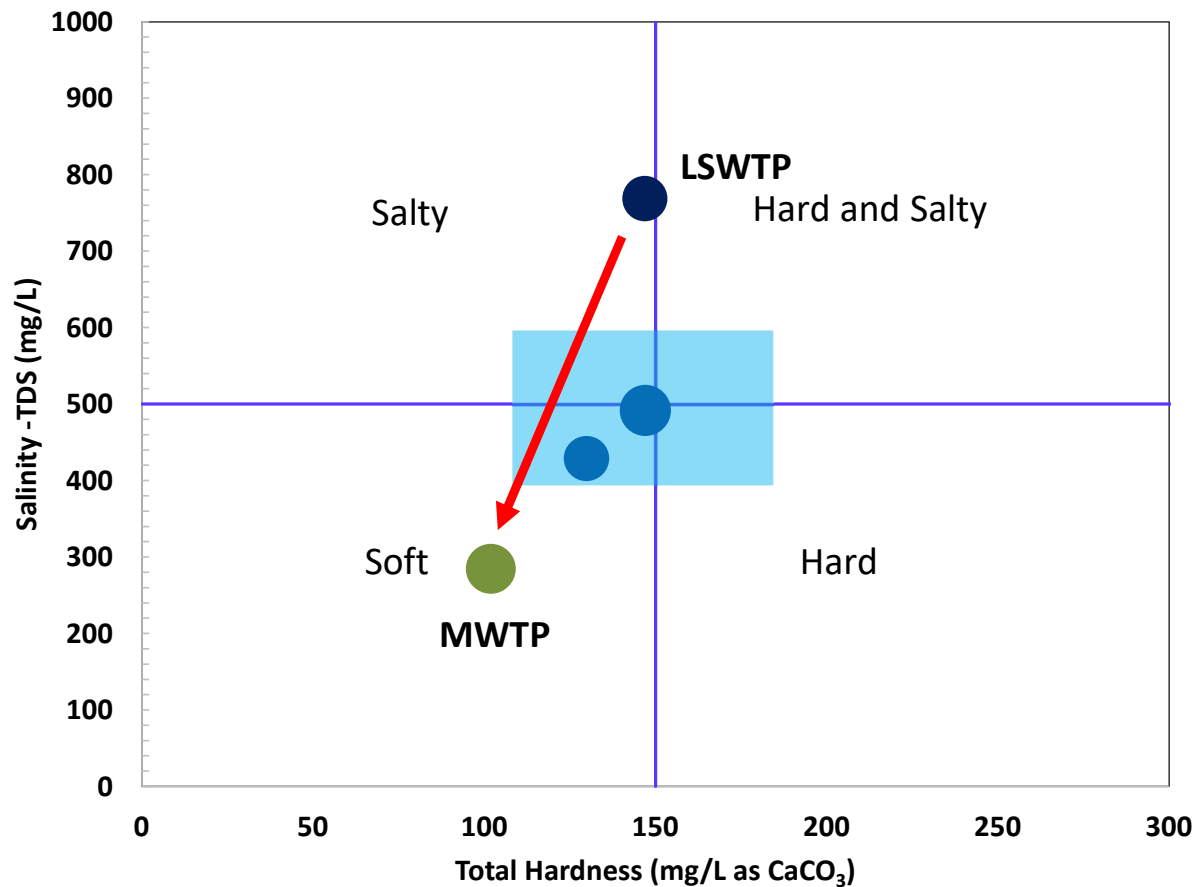


# LSWTP and MWTP Finished Water Quality



➤ The finished water from the Membrane WTP is much softer, lower TDS, and lower TOC.

# LSWTP and MWTP Finished Water Quality



To match the water quality from the MWTP, LSWTP will have to:

1. Lower Total Hardness
2. Lower TDS



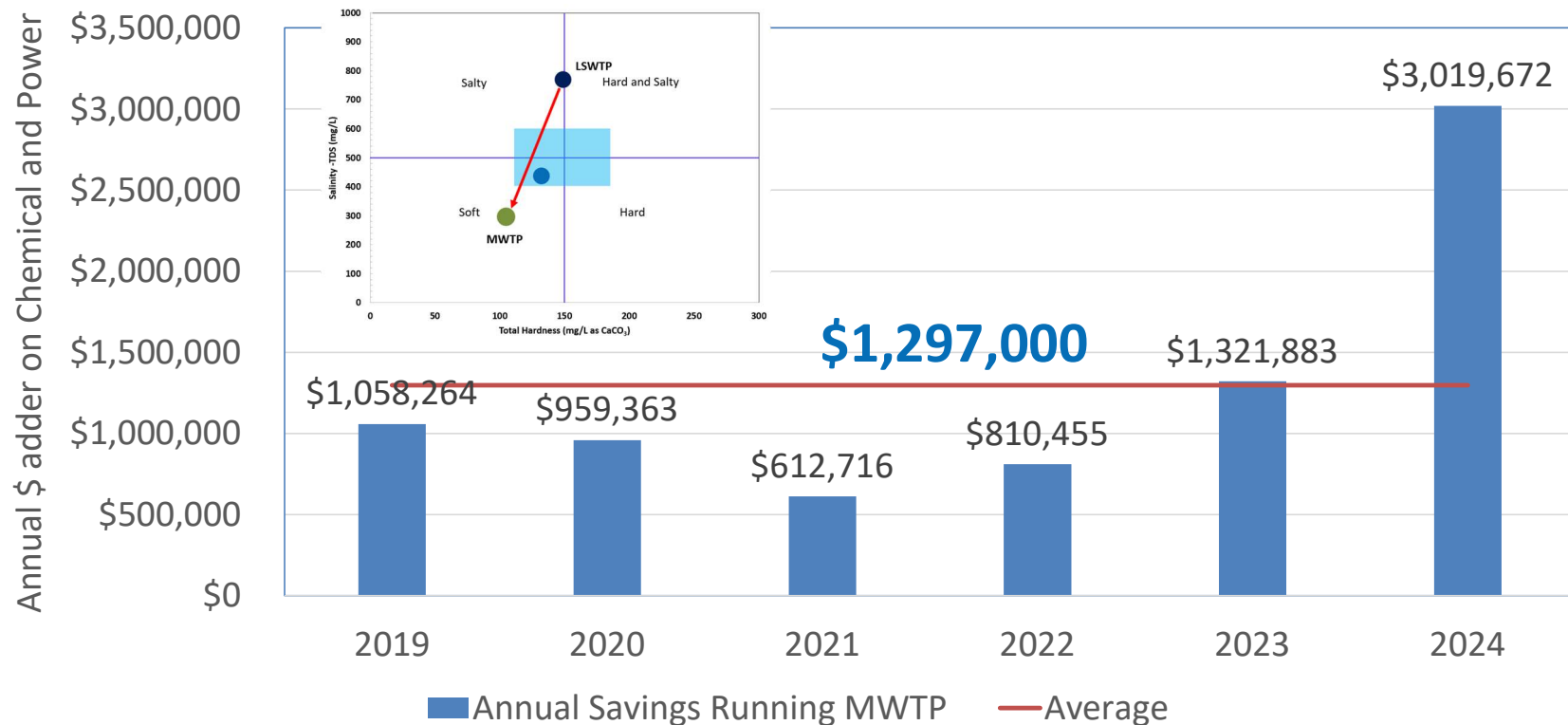
1. Use more lime and soda ash to drive up chemical cost
2. Produce more sludge to increase landfill cost



**What will be the total cost impact?**

# Production Cost Impact

Chemical and Power Annual Cost Adder at LSWTP



# Strategy to Run Both Plants

**Knowing the membrane process is more cost-efficient, the plant staff relies more on the MWTP to manage both water quality and production costs.**

---

- 1. Maintain high production** at the membrane water treatment plant (WTP).
- 2. Transfer RO permeate** to the lime-softening WTP to support overall system performance.
- 3. Slightly elevate total hardness** in the effluent from the lime-softening basins to reduce lime and soda ash usage and associated chemical costs.
- 4. Minimize scaling** in the primary softening basin and downstream processes to help lower operations and maintenance (O&M) expenses.



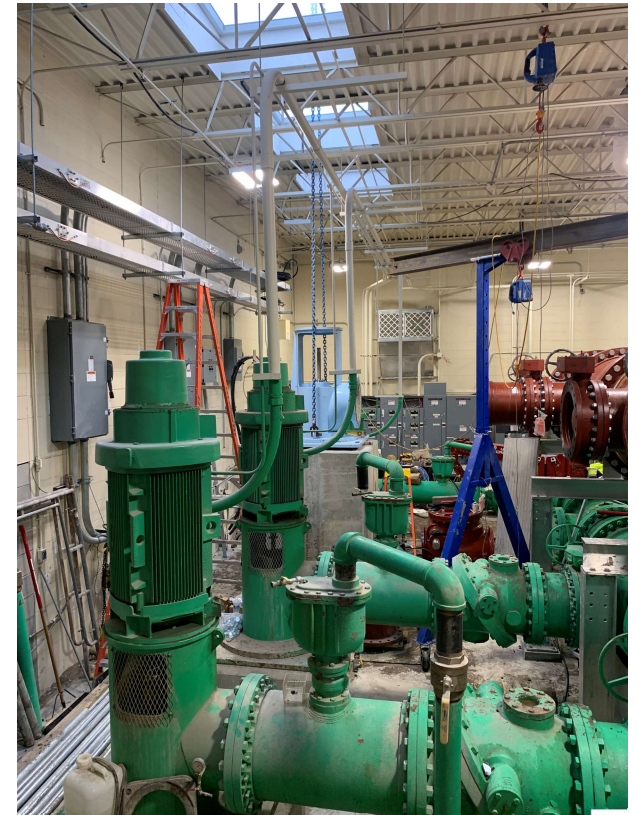
# Supporting Projects

**A series of projects/programs aimed at enabling Fargo WTP staff to operate both plants with optimal cost efficiency and water quality:**

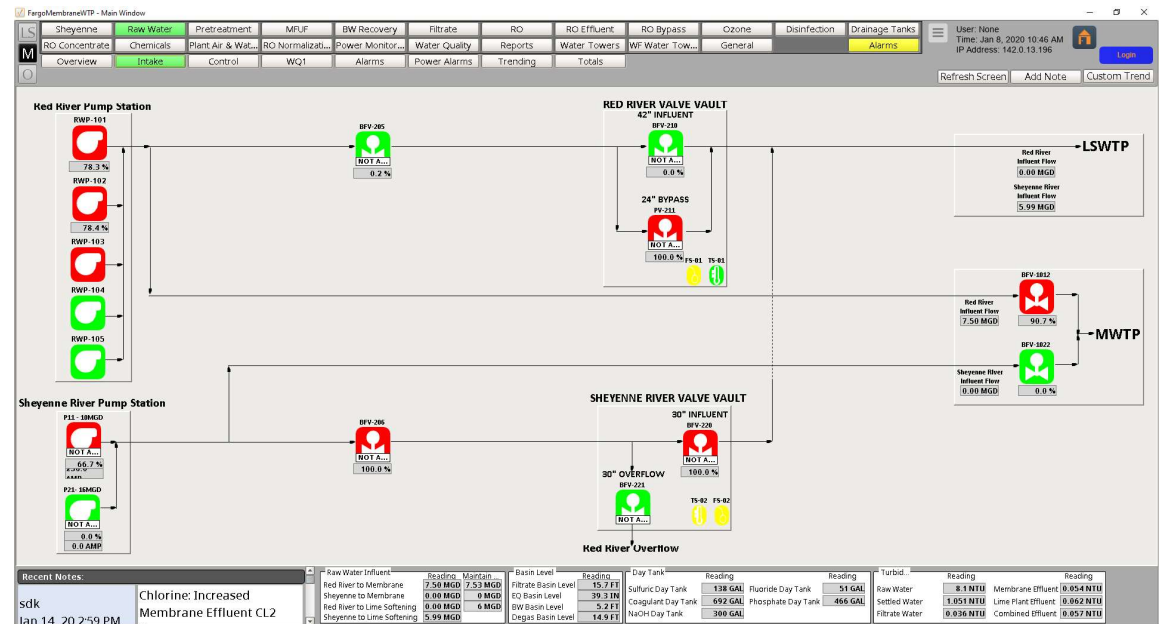
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- 1. Red and Sheyenne Raw Water Intake Projects**
- 2. Raw Water Meter/Valve Vault Project (*with photos*)**
- 3. Grow Our Own Staff**
  - Routine Staff Training Program
  - Conferences/Workshop
- 4. Empowering our staff to develop innovative solutions.**

# Supporting Projects – Intake Projects



# Supporting Projects – Raw Water Valve Vault





# Supporting Projects – Routine Training Program



# **Plant Innovations and Operations Creativities to Get the Job Done**

# Membrane Replacement Schedule

**1**

## **Accelerate UF membrane replacement schedule:**

- Release the stress on the operation team to repair broken fibers
- Increase MWTP treatment availability to manage the overall cost and production

**2**

## **Steady pace to replace RO membranes**

- Competitive RFP to reduce the replacement cost
- Manage RO permeate quality



# Select Appropriate Technology

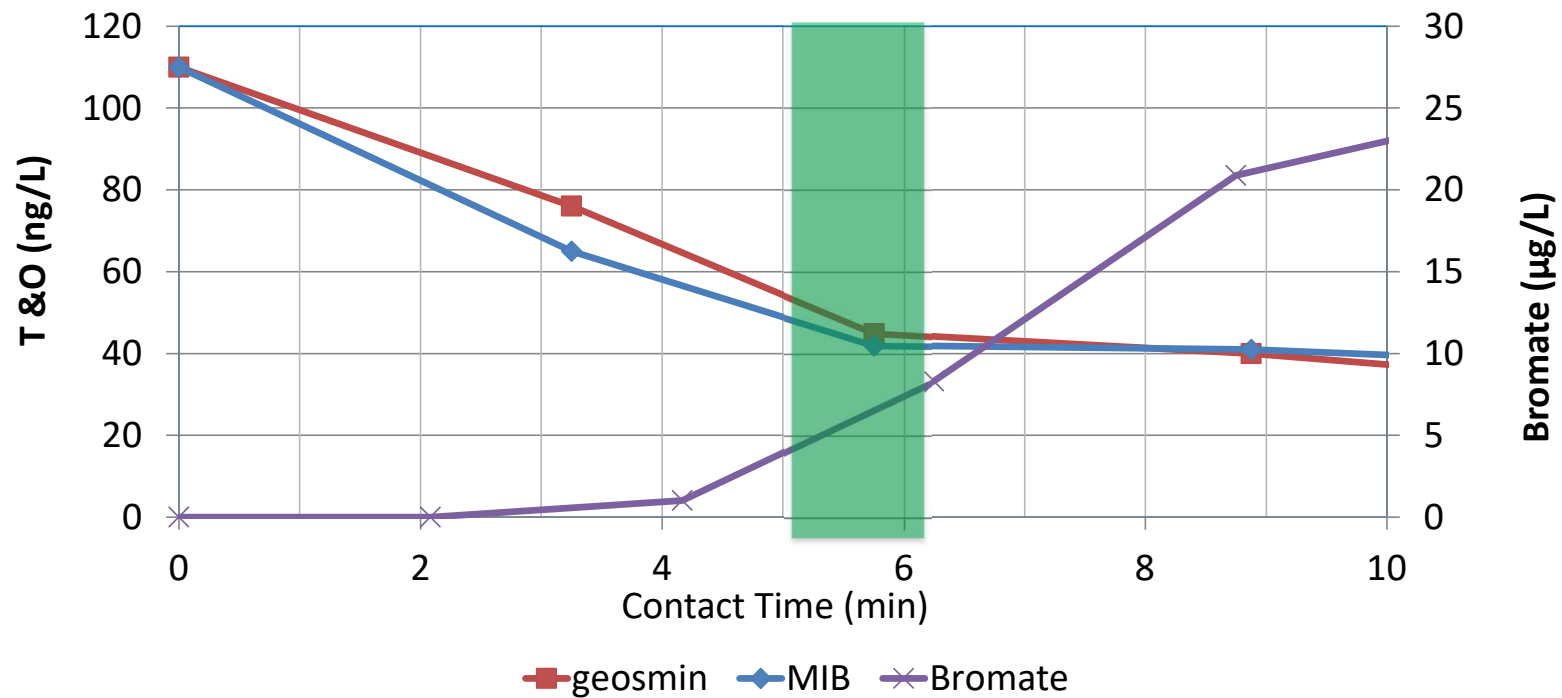
## 3 Liquid Oxygen (LOX) –VSA Installation

- Annual usage reduction: 624 tons
  - 2017-2018 (Ave): 1,065 tons
  - 2022-2023 (Ave): 441 tons
- Cost reduction: **\$88,875** in 2024.



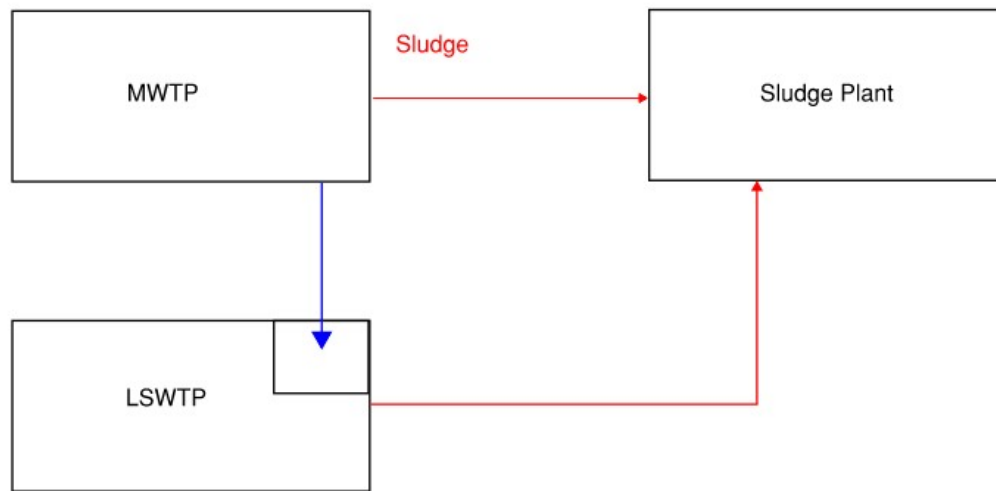
# Data Driven Operation Decision to Improve Water Quality

## T&O Removal and Bromate Formation Mitigation



*Fargo WTP T&O Ozone Pilot Study (2013)*

# Creative Plant Operation – Sludge Thickening

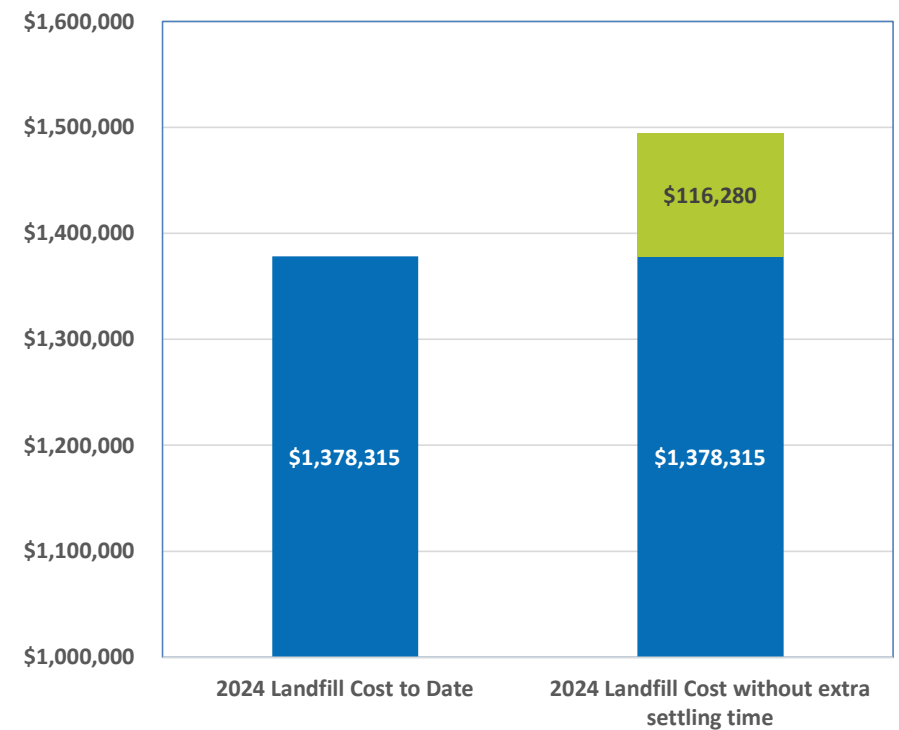
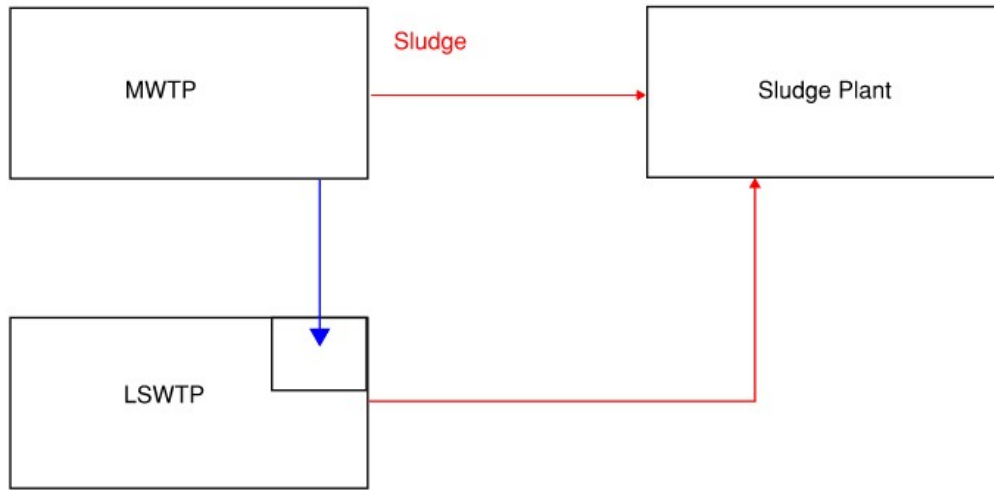


Solids content increased from 37% up to 41% on an average.

**What is the impact?**



# Creative Plant Operation – Sludge Thickening



**Compared to 2023 Data**

# Staff Go Above and Beyond

**0.02 N Standard acid solution  
for online hardness and  
alkalinity instrument:**

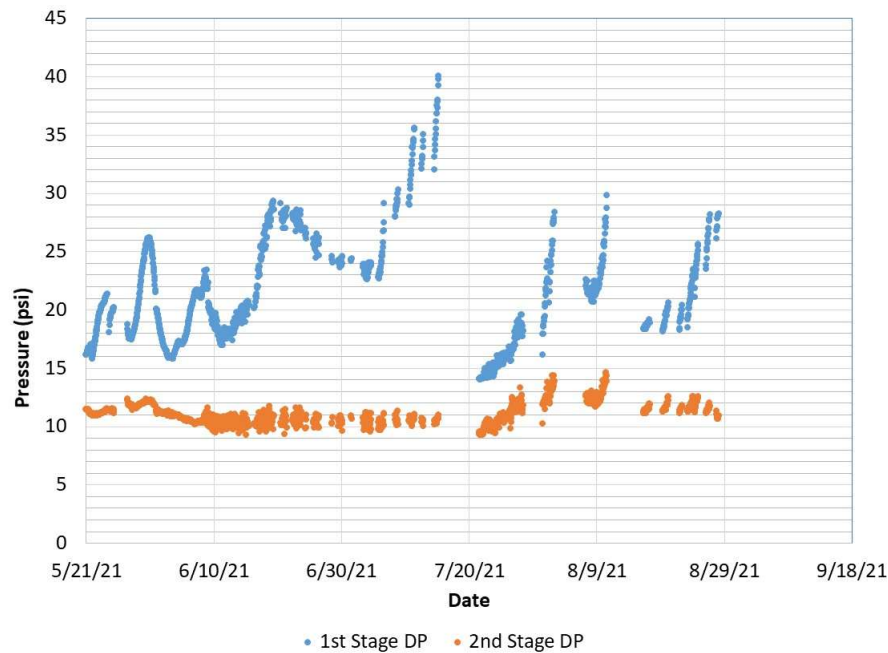
## **Home-Made**

- 40% sulfuric acid: \$0.53-\$0.77/lb
- Weekly Usage: 80-100 mL
- Annual Cost: \$6-\$9

**Annual Saving: \$40,000**



# Staff Go Above and Beyond



1. Feed chlorine to Filtrate wetwell
2. Feed sodium bisulfite to quench chlorine residuals
3. Relocate anti-scalant feed point
4. Install an inline mixer
5. Feed hydrogen peroxide to RO feed
6. Test various anti-scalants
7. Test a biocide (NSF approved)
8. Evaluated various CIP regimes
  - 1) Circulate time/flow rate
  - 2) Soaking time
  - 3) CIP chemicals
9. Rinse the 1<sup>st</sup> stage lead elements
10. Replace the RO element interconnectors
11. Replace RO brine seals
12. Relocate 1<sup>st</sup> stage lead RO elements
13. Blackboxes monitoring
14. Bacteriological testing (HPC)
15. Membrane autopsy
16. Cleaning study



# Cost Efficiency

**1. MWTP Design: \$1.30 million annually**

- RO Transfer line
- Biological GAC after ozone-peroxide
- Cost information analysis tools

**2. LSWTP Solids Production Avoidance (\$1.7-\$3.3 million)**

**3. Ozone: Phase 2: \$60,000 annually**

- VSA System Installation

**4. MWTP Sludge Settling: \$100,000-\$150,000 annually**

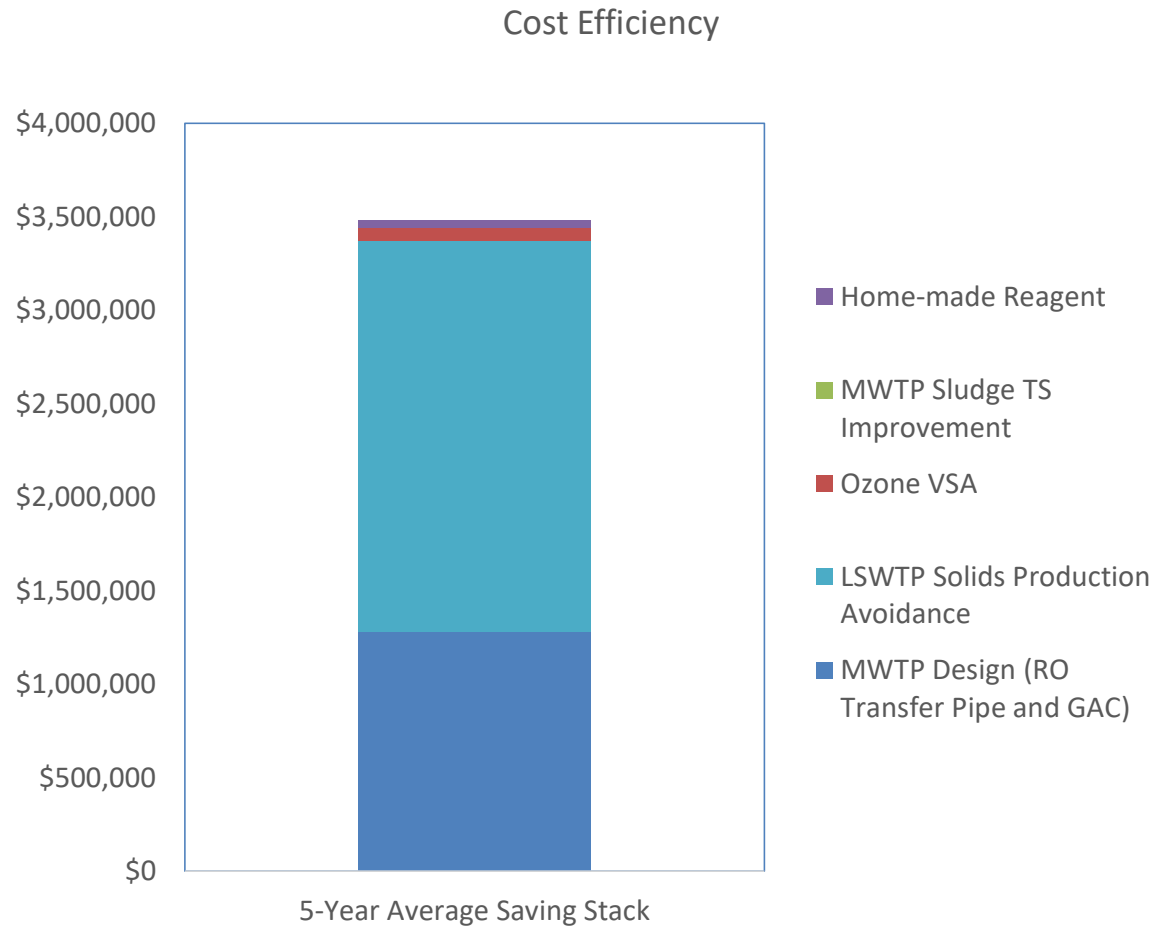
- 2024 to landfill: 37% → 41%
- Hauling less water
- Less sludge plant polymer use (\$38,000)

**5. Analyzer Reagent Savings: \$40,000 annually**

**6. What's left: More than \$200,000 annually**

- Increase MWTP/RO operation
- RO CIP Optimization
- Lime softening WTP process optimization

# Cost Efficiency



# What is in the Near Future?

# Master Planning: Next 2-3 Years

**Every 7 years or so....**

## **Assess Whole Water System**

- Water Plant
- Raw Water Supply
- Water Distribution System
- Future Financial Needs

## **Work In-progress**

- LSWTP Processes Rehab
- Treatment Process Optimization (CO<sub>2</sub>, Ozone,...)
- City-wide AMI project
- Lead Service Line Replacement



# QUESTIONS? THANK YOU!

T. Hall, Water Utility Director, Fargo  
Q. Chang, Senior Advanced Technical Specialist, AE2S

